

Ammonia-salt large temperature jump analysis

MI meeting

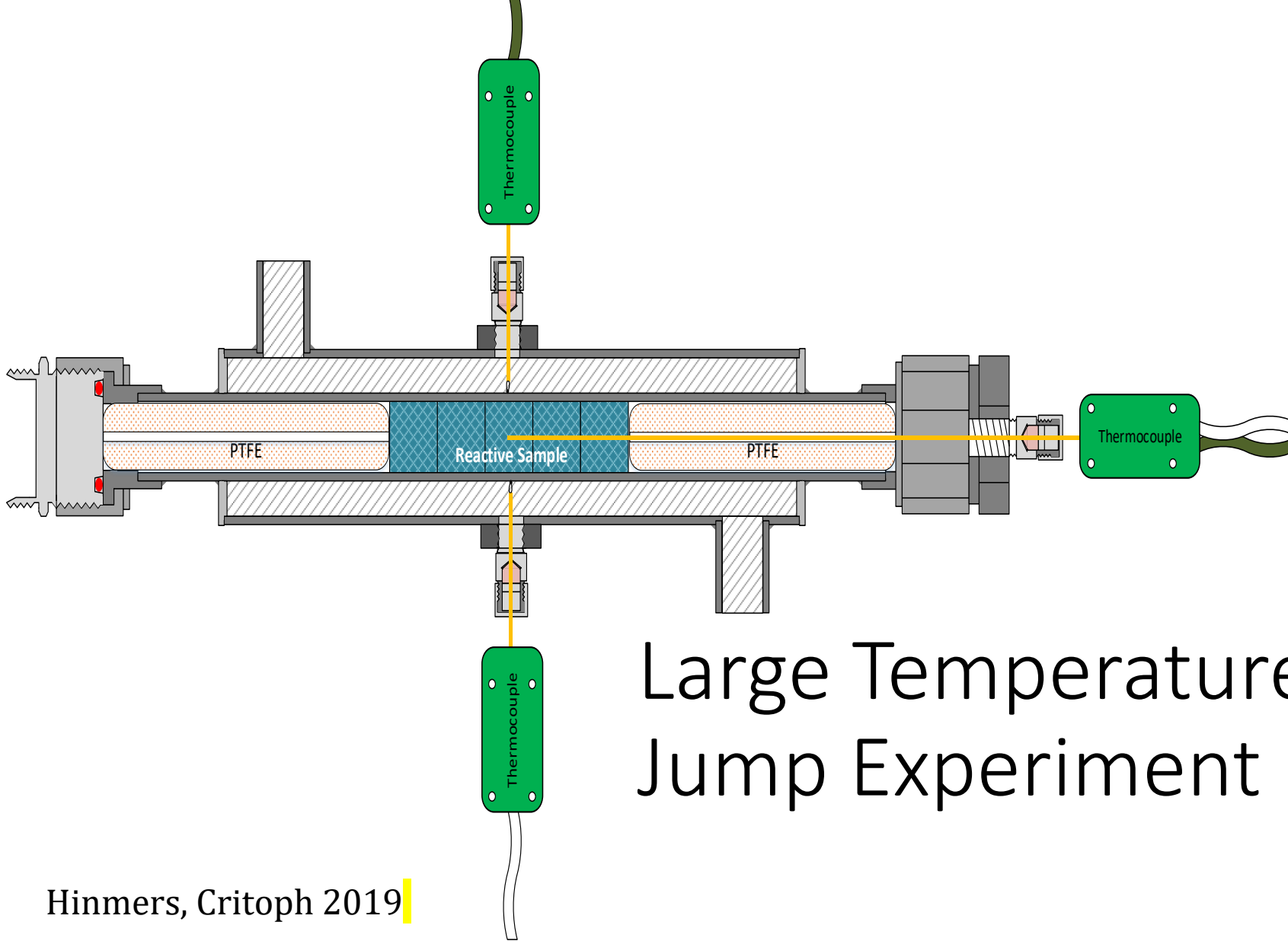
14th December 2020



Outline

- Large temperature jump tests
- Elusive Equilibrium data
- Initial analysis
- Some of the challenges

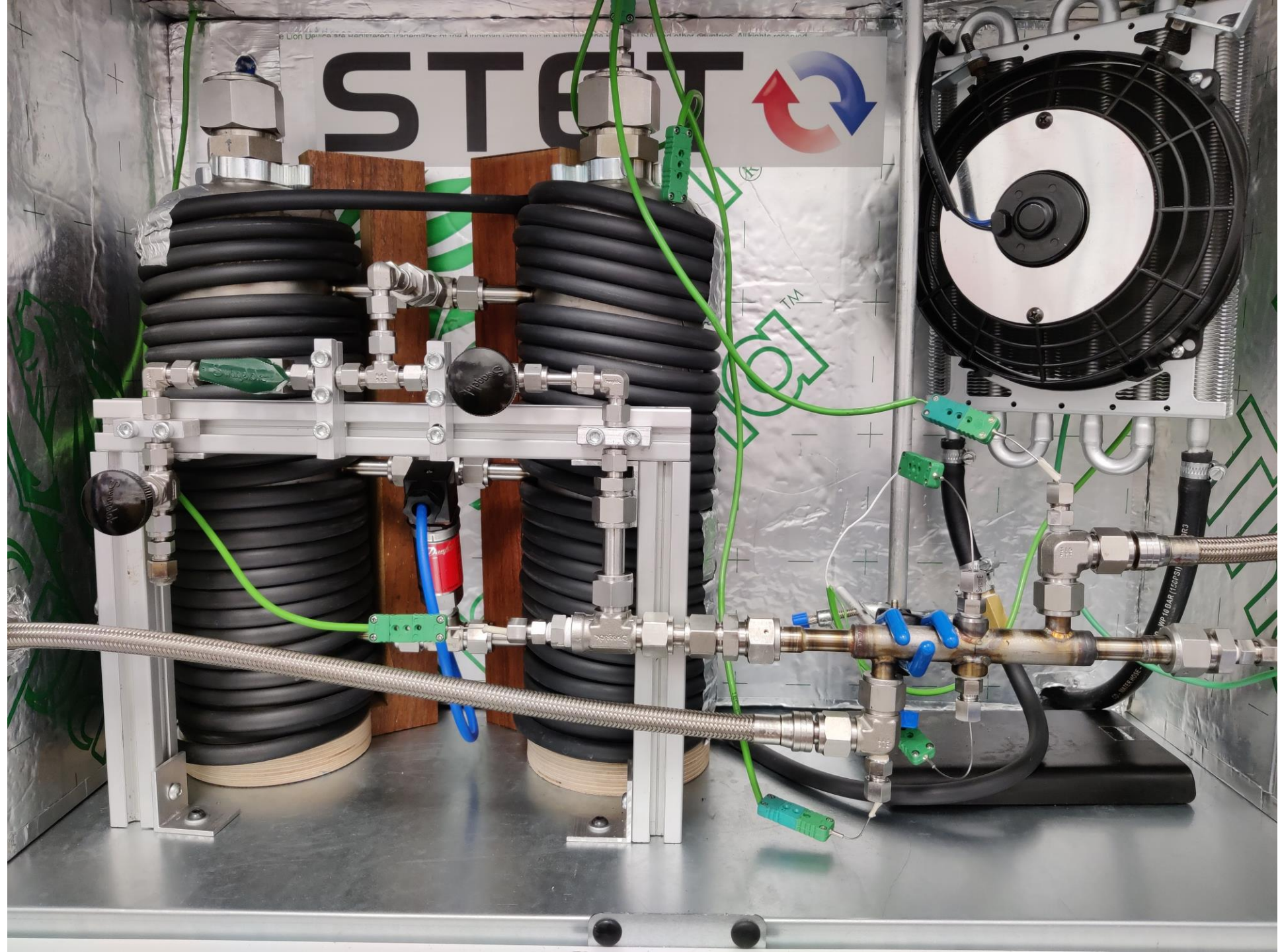


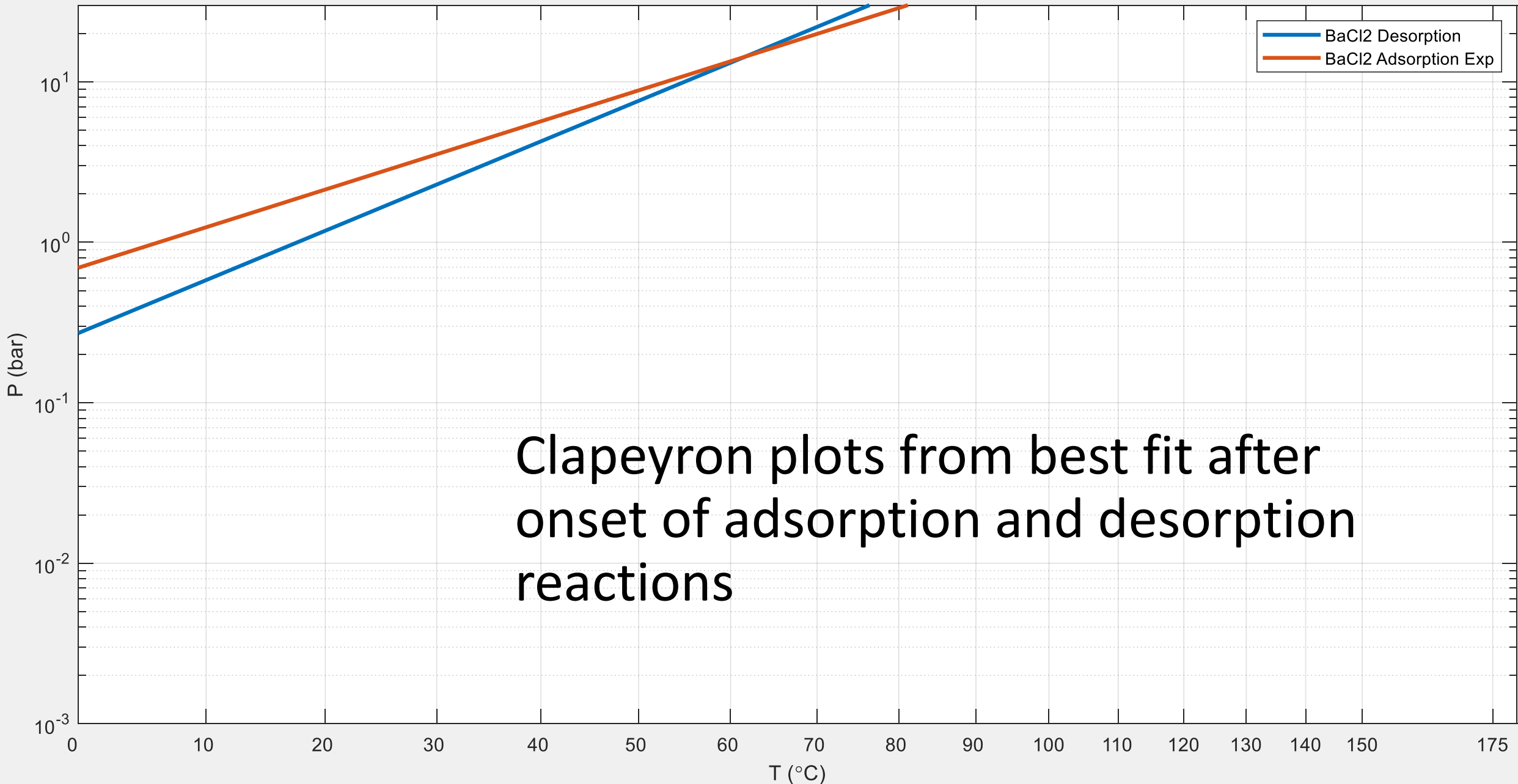


Large Temperature Jump Experiment

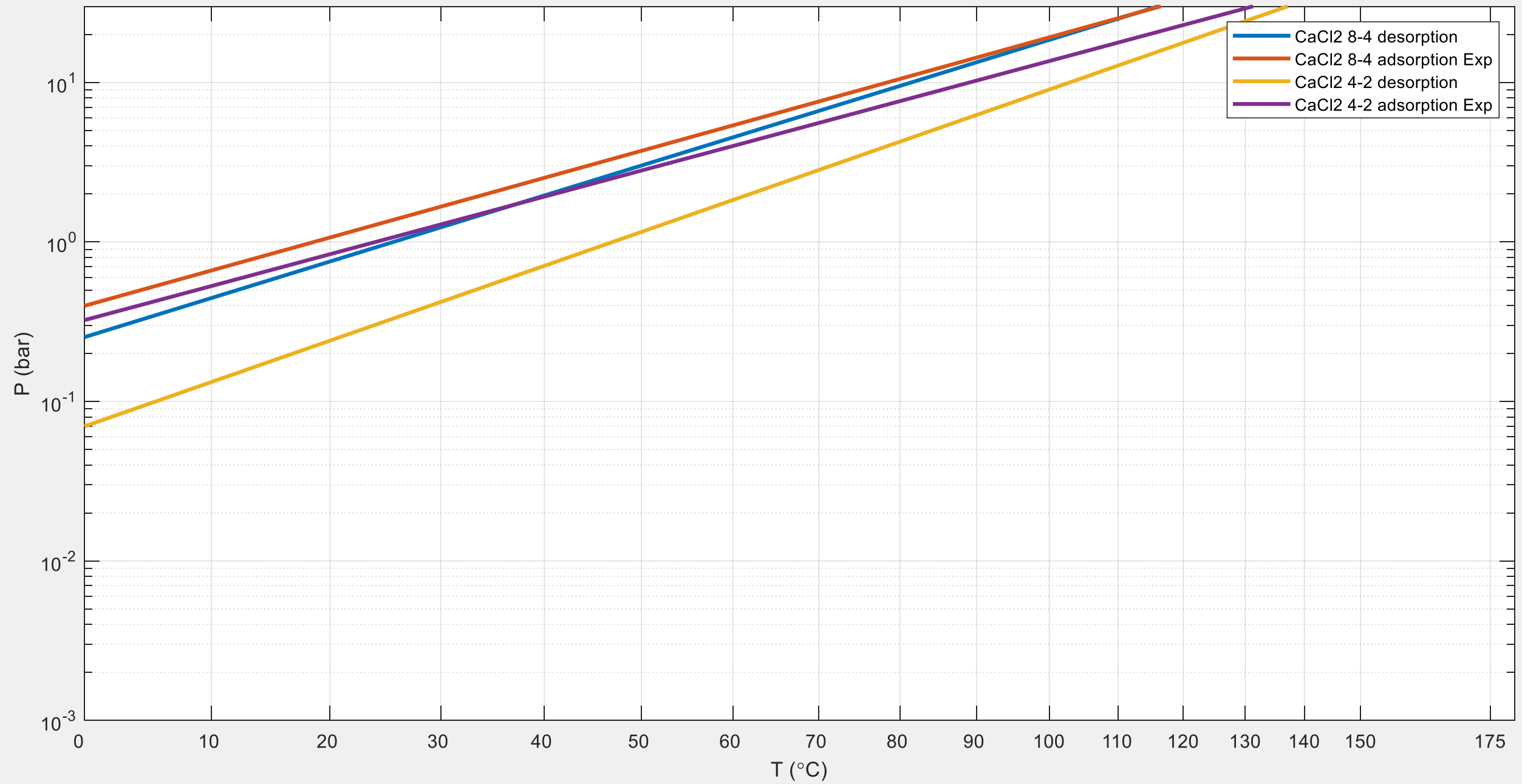
Hinners, Critoph 2019

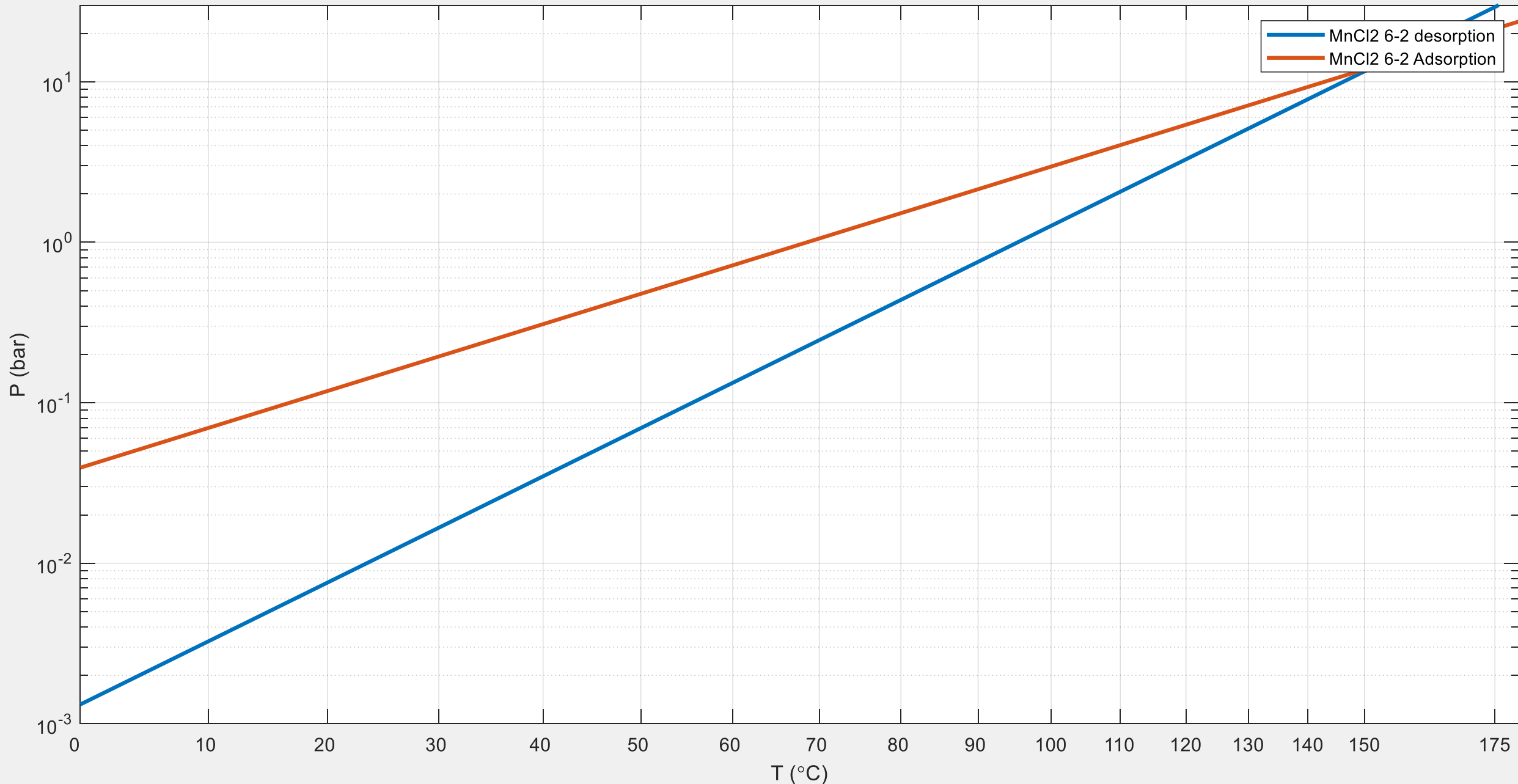


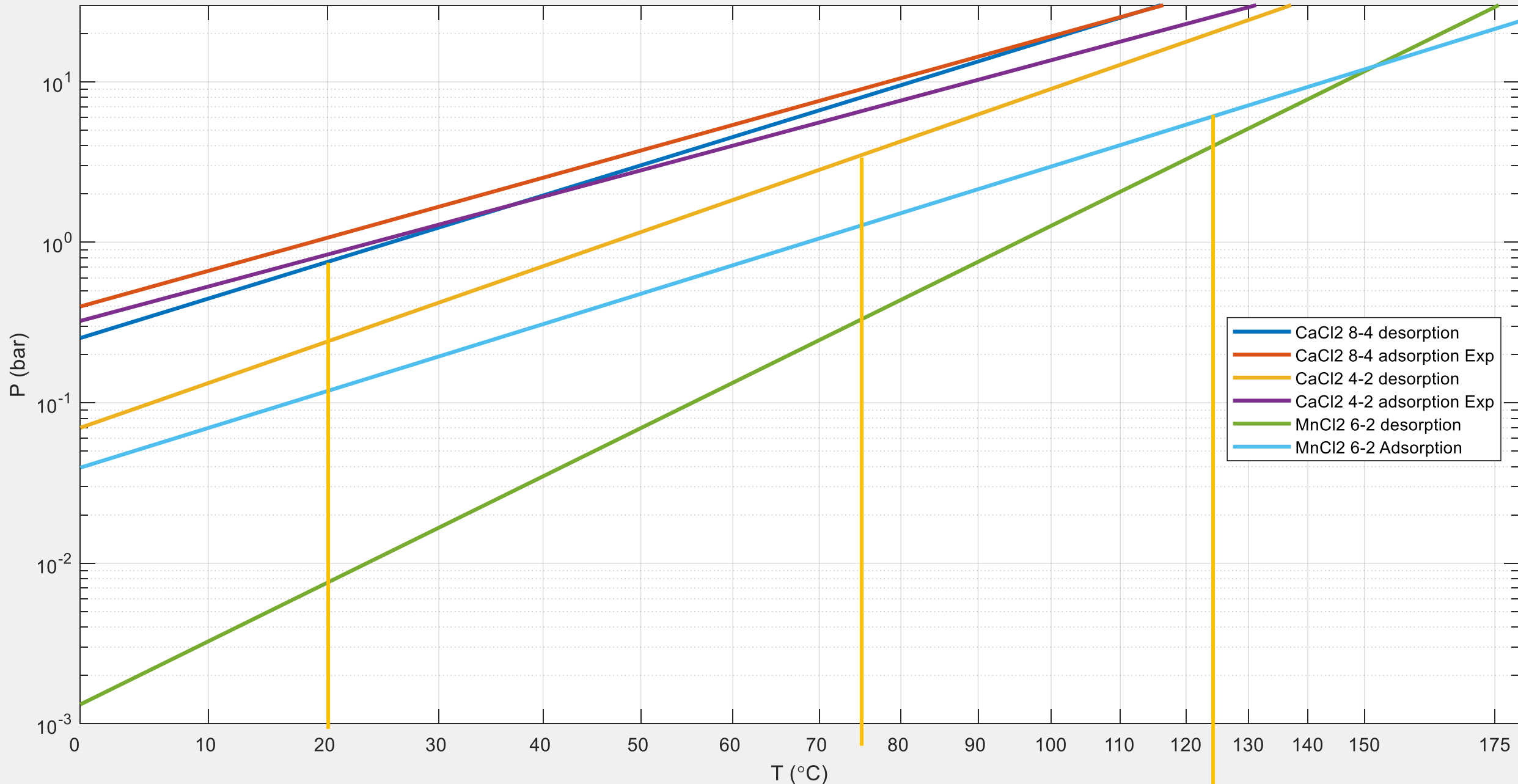




Clapeyron plots from best fit after
onset of adsorption and desorption
reactions

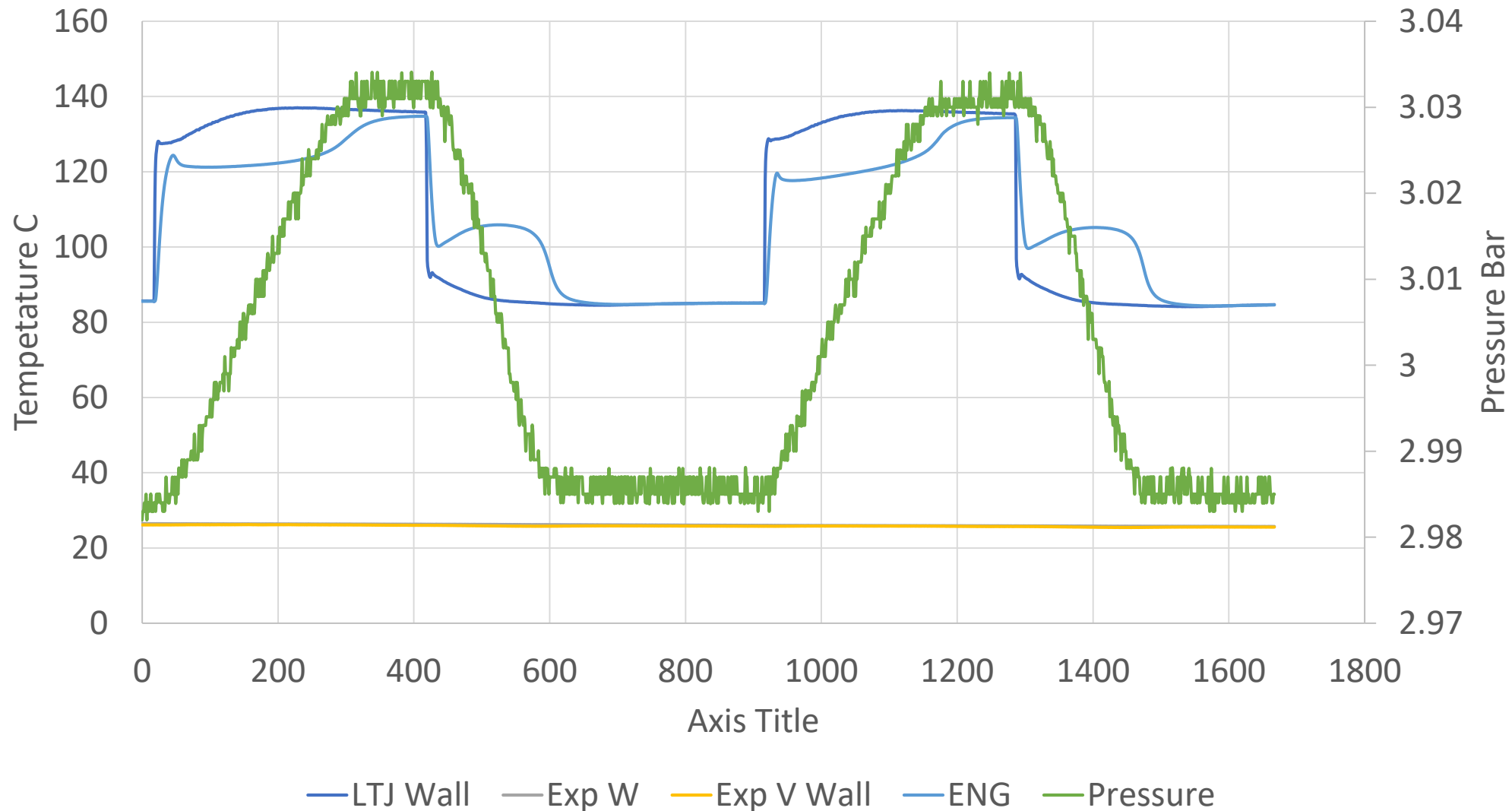






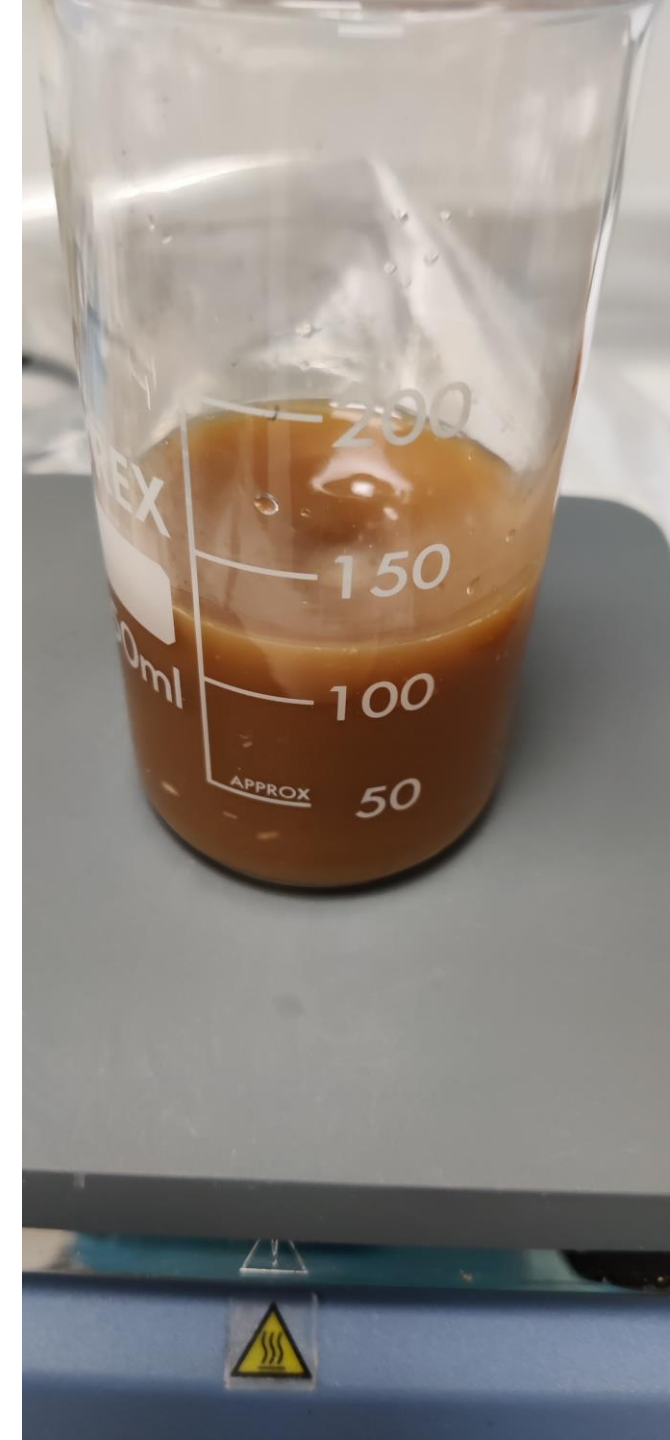
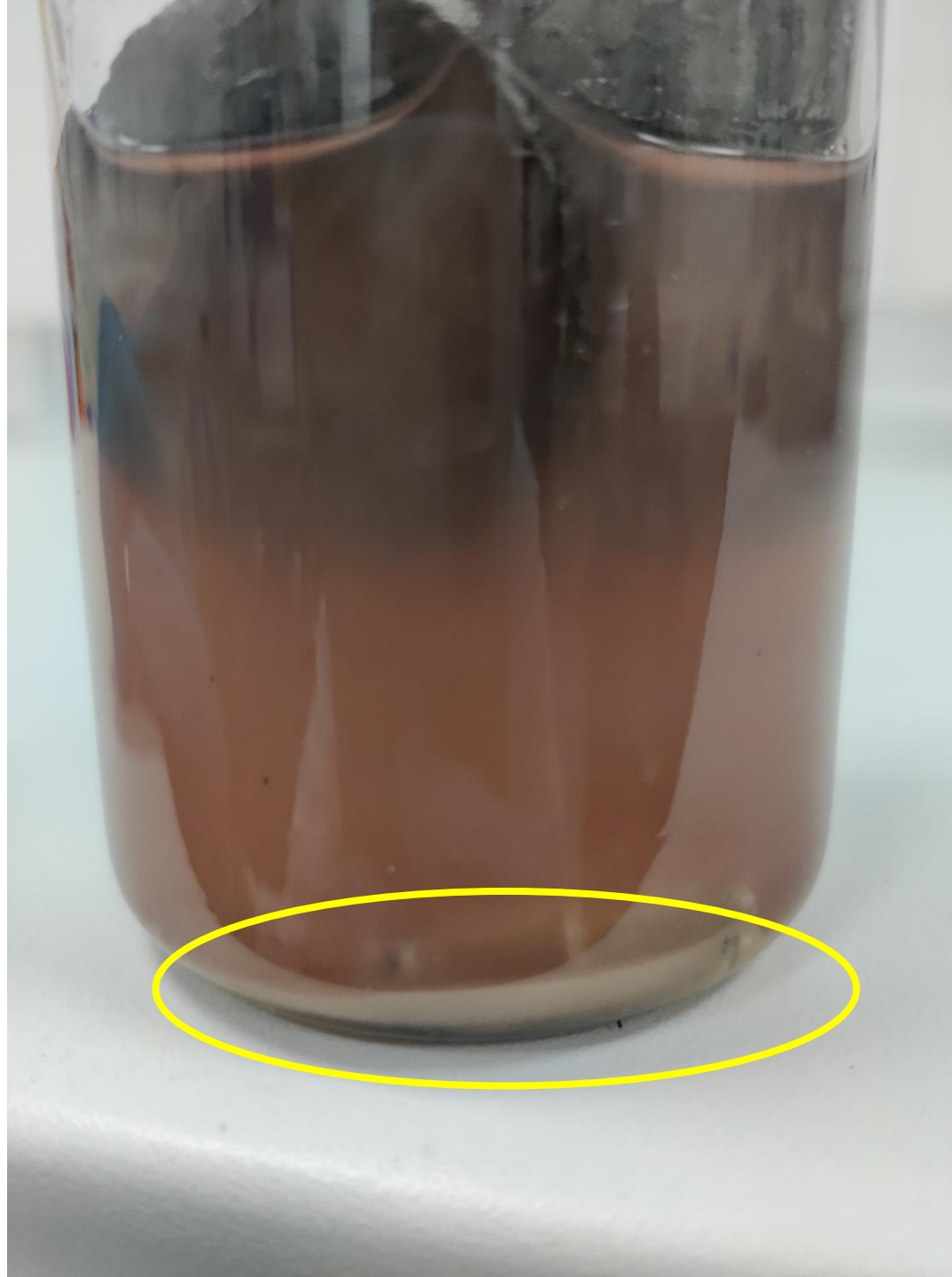
Challenges of working with salts

3 bar MnCl₂ Cycles



MnCl₂ Challenges

- Appears to have a notable lower 'active fraction' of salt than CaCl₂ and BaCl₂ @0.6
- Pellet form is prone to oxidising and precipitating out of solution (including with ethanol)
- Perhaps MnO₂ forms some of the 'inactive salt fraction'





Accurate Thermocouple Readings

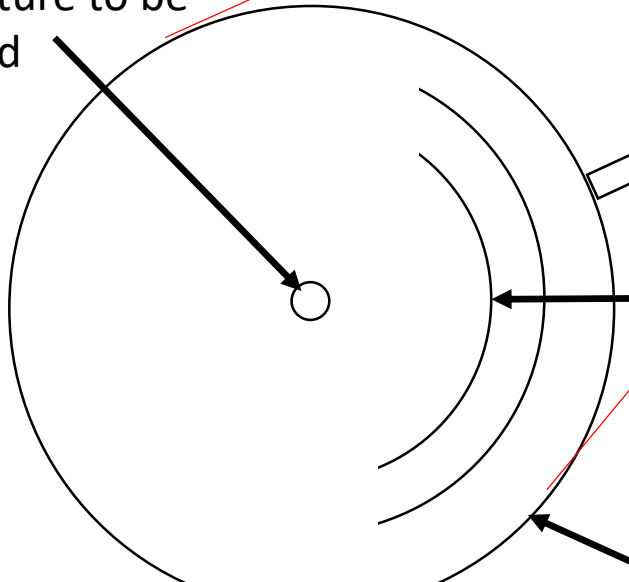
- Grounded thermocouples working as a pair are very tricky
- They can drift/expand due to heating so to ensure contact is difficult particularly within the ammonia volume
- Data acquisition with the pressure transducer into the same module or device was also challenging, as on a standard DAQ device it would put voltages across the device as well as voltage across the rig itself
- Addressed with separate devices and grounding to avoid noise-
 - At one point, flickering lights appeared to produce a frequency that could be picked up in the noise from the mains earth!

Modelling success

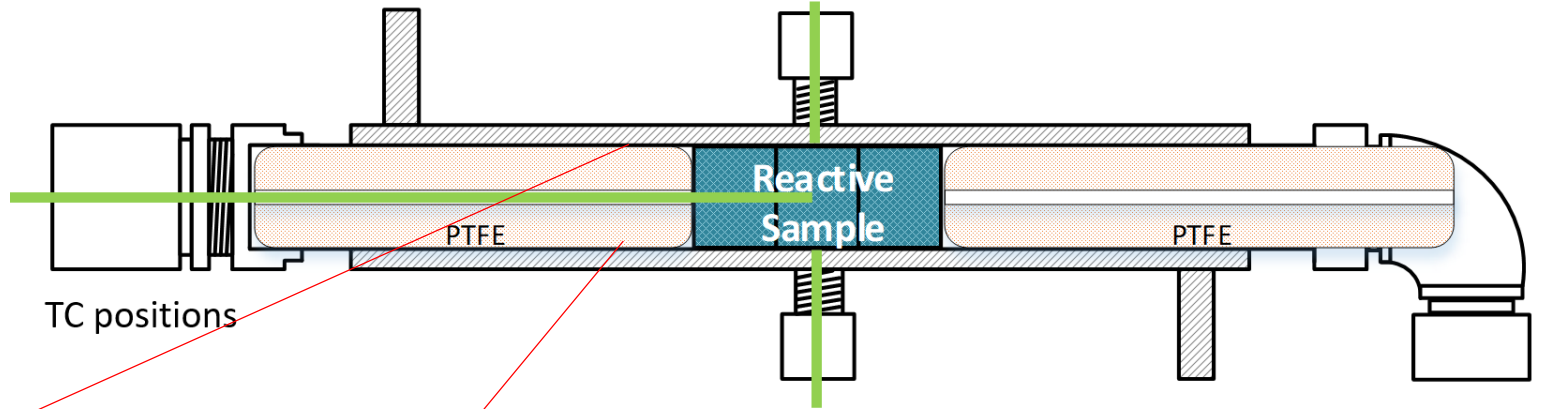
LTJ Test modelling

1-d axi-symmetric model

Centre thermocouple temperature to be simulated



Large Temperature Jump Reactor



½ inch pipe centre

1 inch pipe jacket

PTFE to fill heated volume

O-ring Swagelok face seal fitting

Pressure to be simulated

n elements of ENG and salt at radius r
Wall at measured temperature (boundary condition)

Similar to the linear form used by SJTU

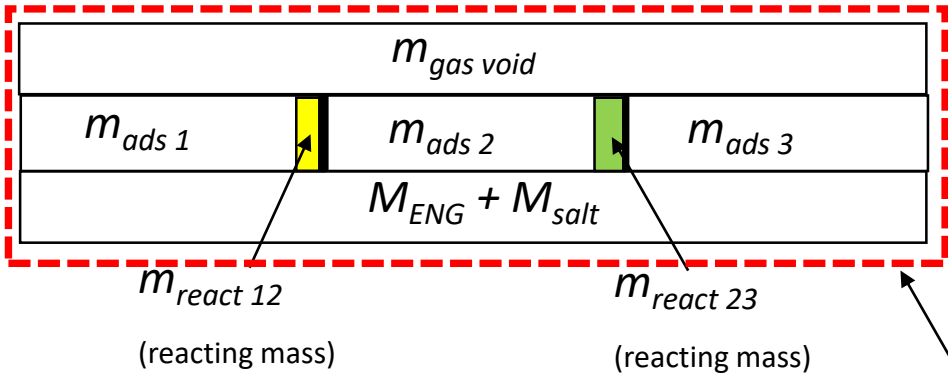
$$\frac{dX}{dt} = (1 - X)^y A \frac{p_{eq} - p}{p}$$

Mazet, Amaroux & Spinner 1991

Reaction Engineering

$m_{ads\ 1}$	$m_{ads\ 2}$	$m_{ads\ 3}$
$m_{salt\ 1}$	$m_{salt\ 2}$	$m_{salt\ 3}$

Time t



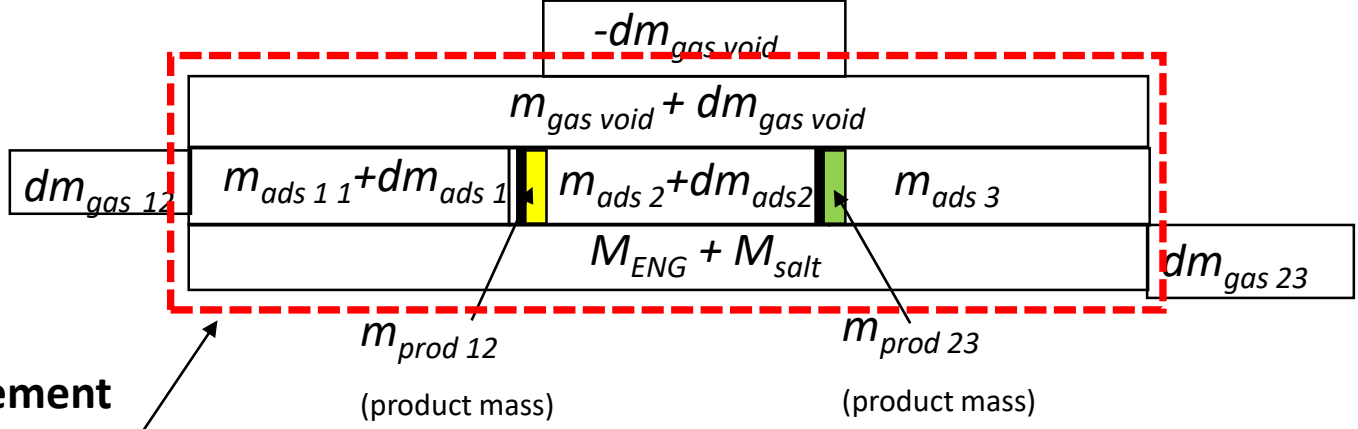
Time t

Bob's derivation of the Energy Balance:

$$dT = \frac{dQ - dm_{gas\ 12}\Delta h_{12} - dm_{ads\ 12}pv_{ads} \left(1 - \frac{B}{A}\right) - dm_{gas\ 23}\Delta h_{23} - dm_{ads\ 23}pv_{ads} \left(1 - \frac{C}{B}\right) + V_{void} \frac{dp}{1 + dp/T}}{Mc_p + \sum_1^3 m_{ads} c_{v\ ads} + m_{gas\ void} c_{v\ gas} - V_{void} \frac{pT}{1 + dp/T}}$$

$m_{ads\ 1} + dm_{ads\ 1}$	$m_{ads\ 2} + dm_{ads\ 2}$	$m_{ads\ 3} + dm_{ads\ 3}$
$m_{salt\ 1} + dm_{salt\ 1}$	$m_{salt\ 2} + dm_{salt\ 2}$	$m_{salt\ 3} + dm_{salt\ 3}$

Time t + dt



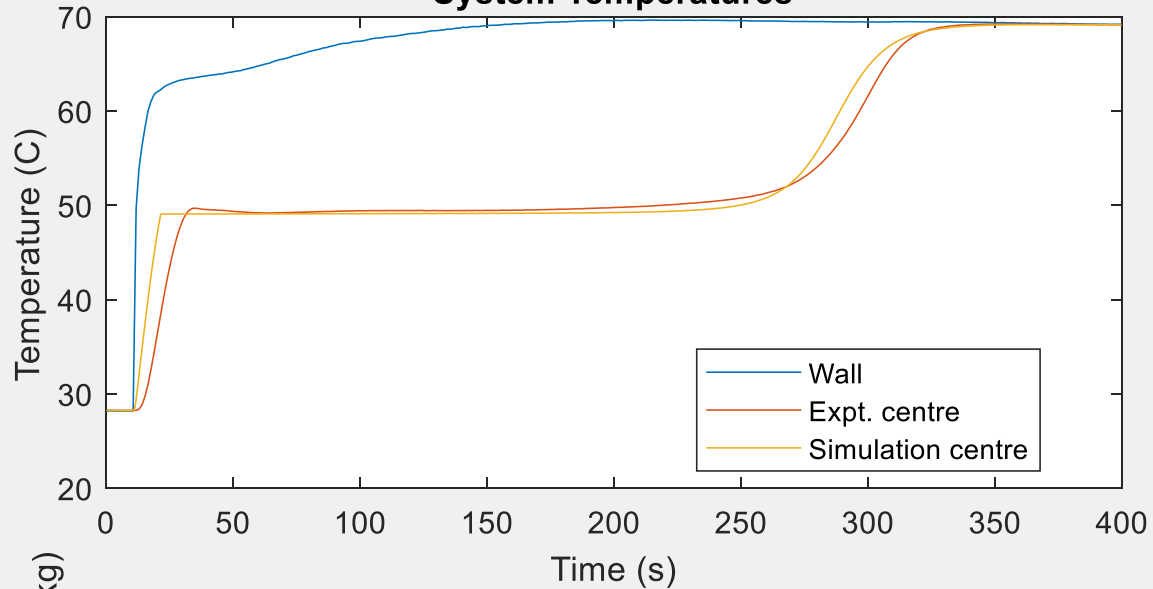
Time t + dt

Element control volume

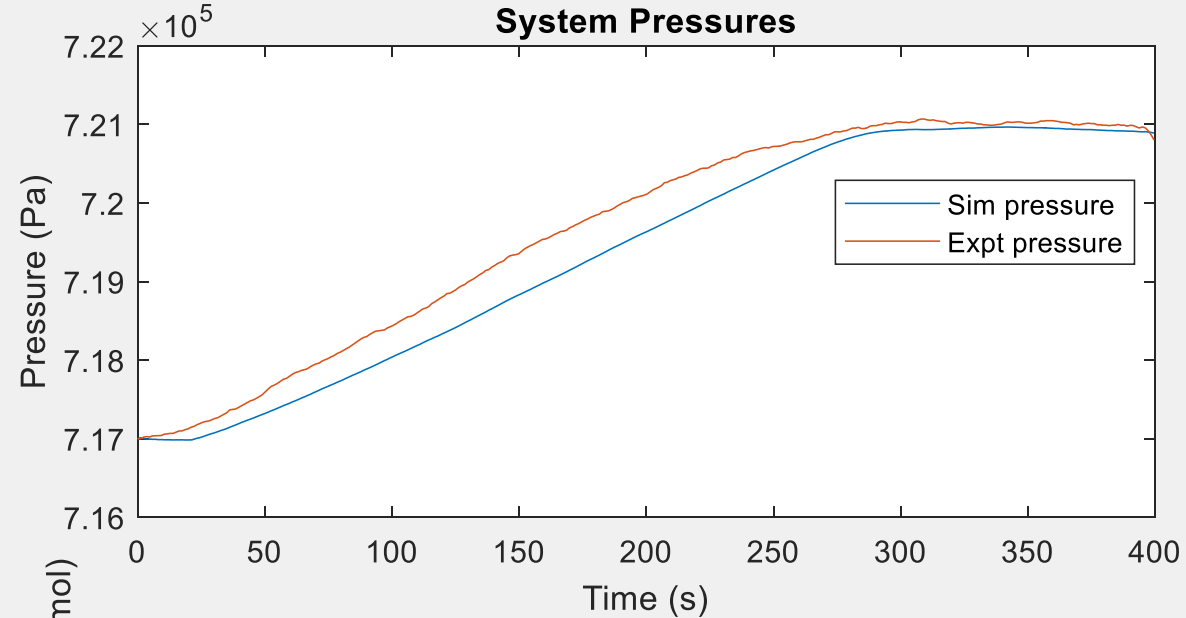
Proof is in the plotting.....

Barium Chloride 7bar LTJ test

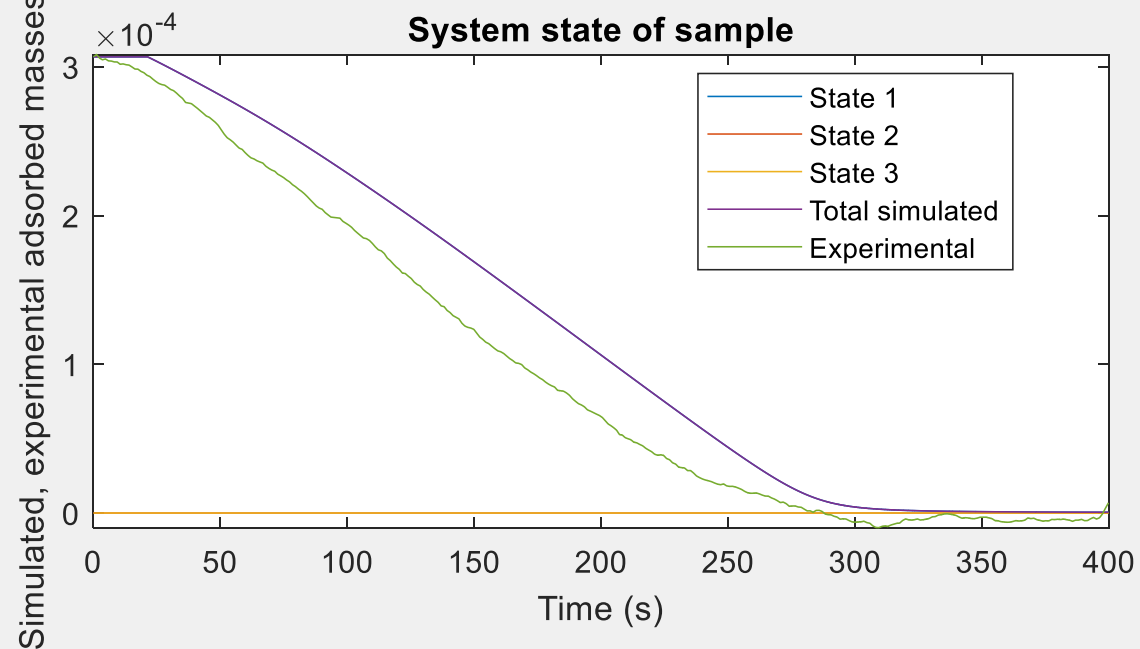
System Temperatures



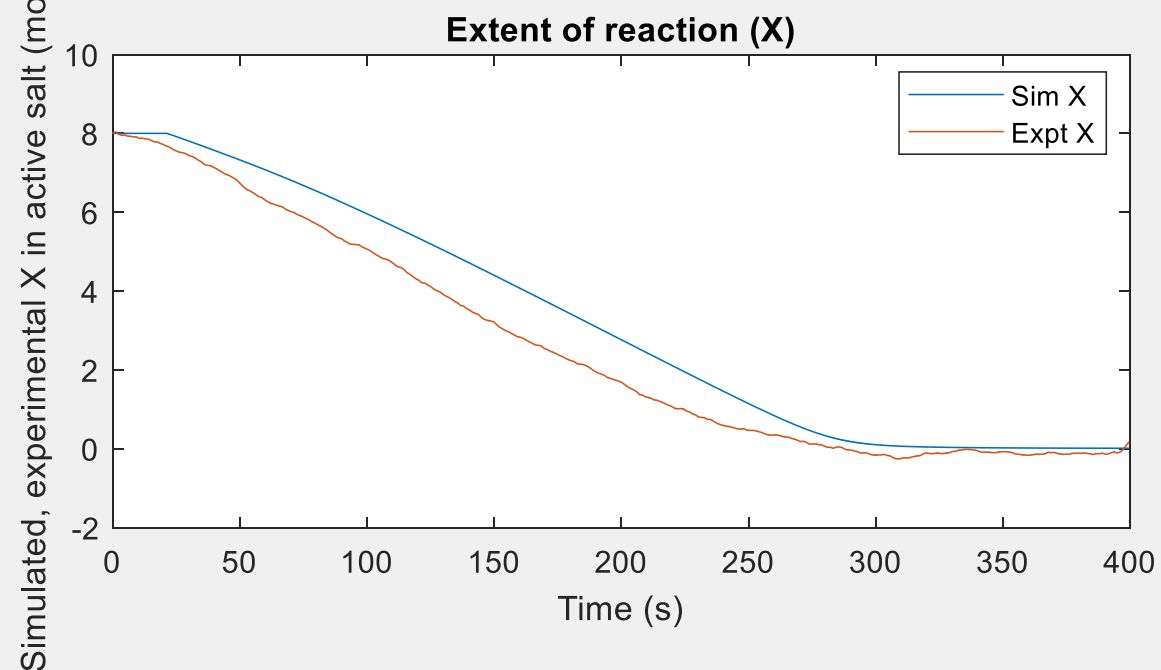
System Pressures



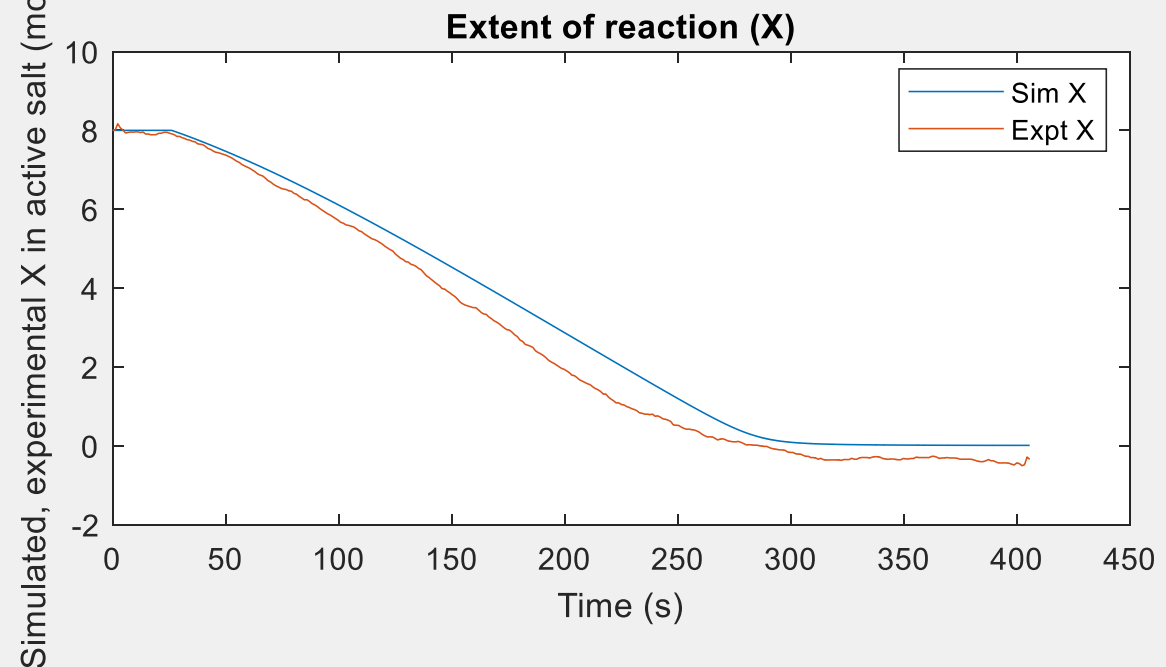
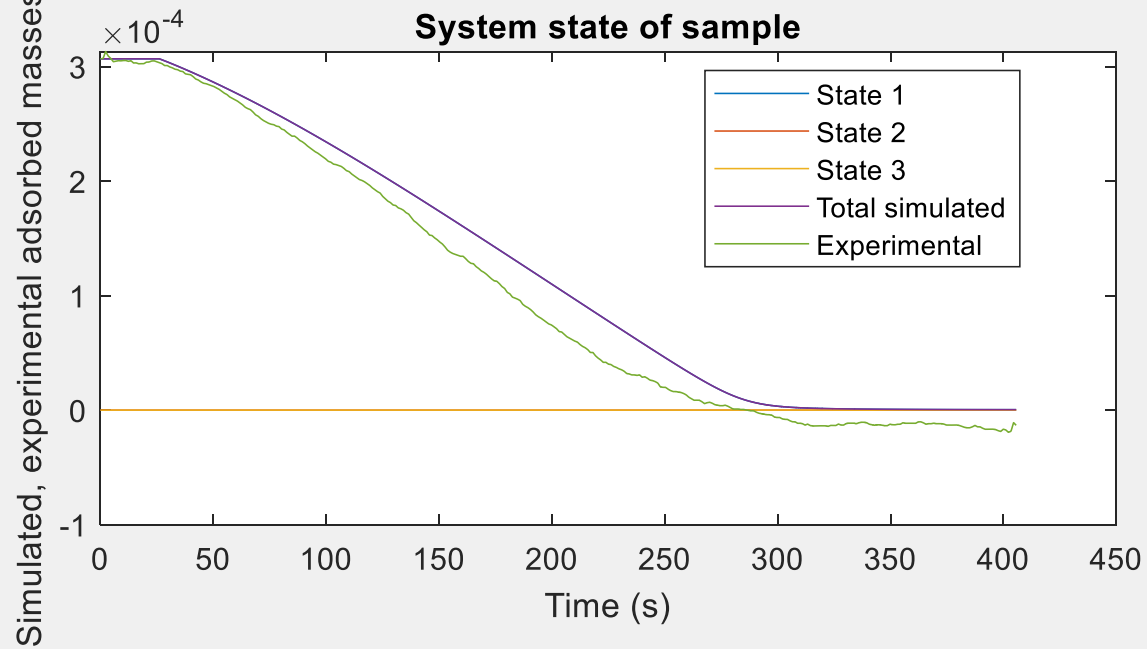
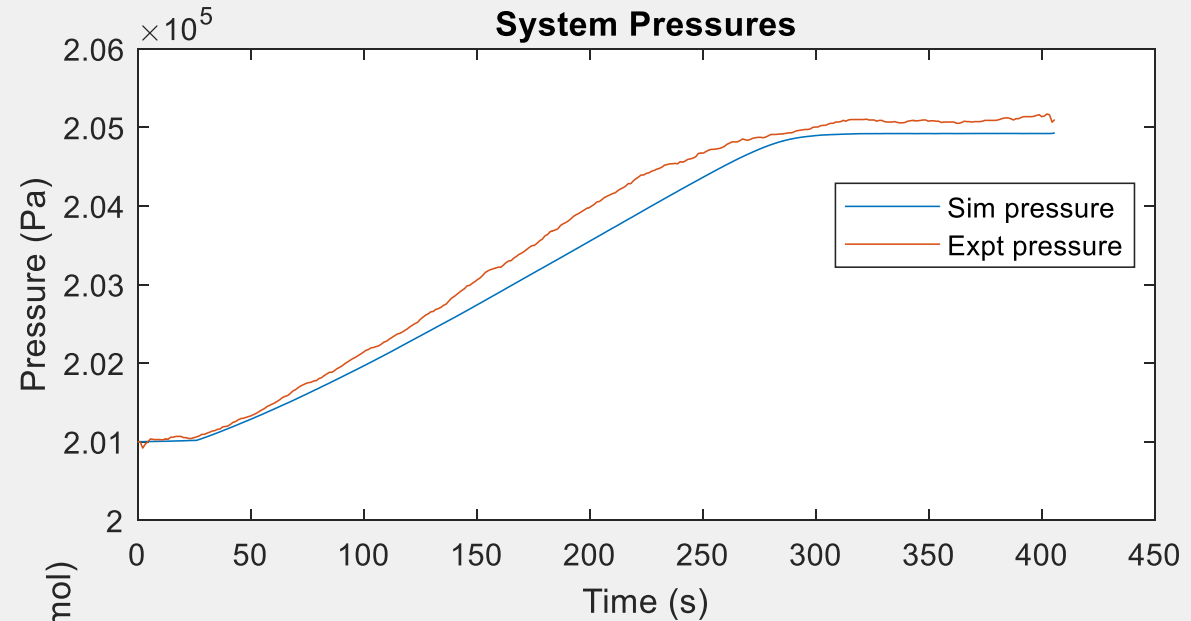
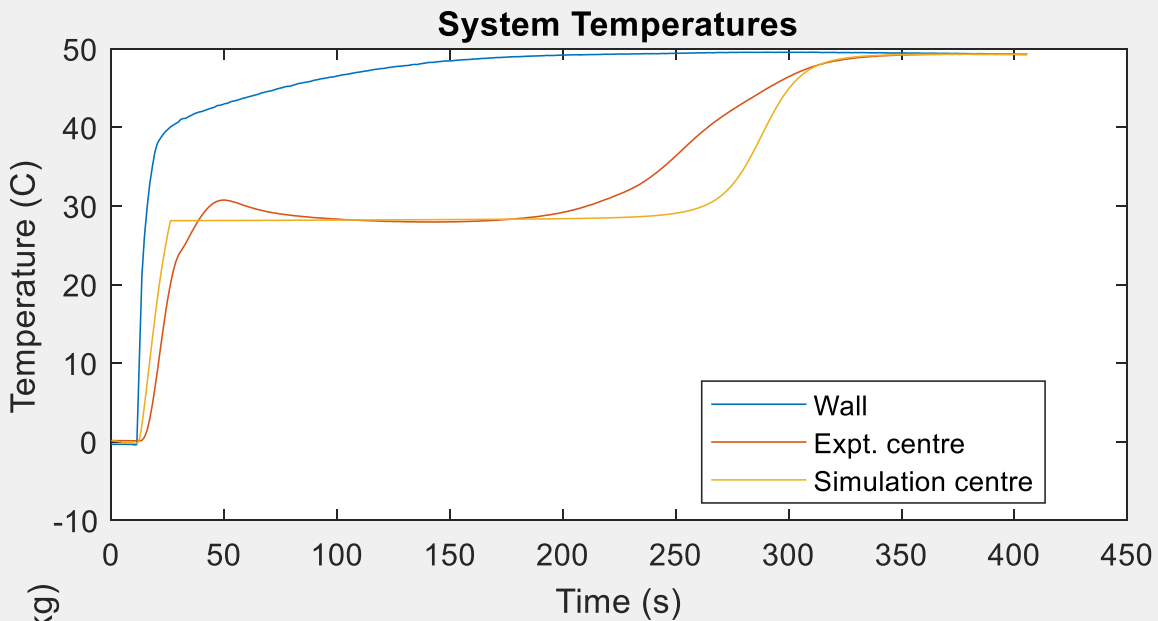
System state of sample



Extent of reaction (X)

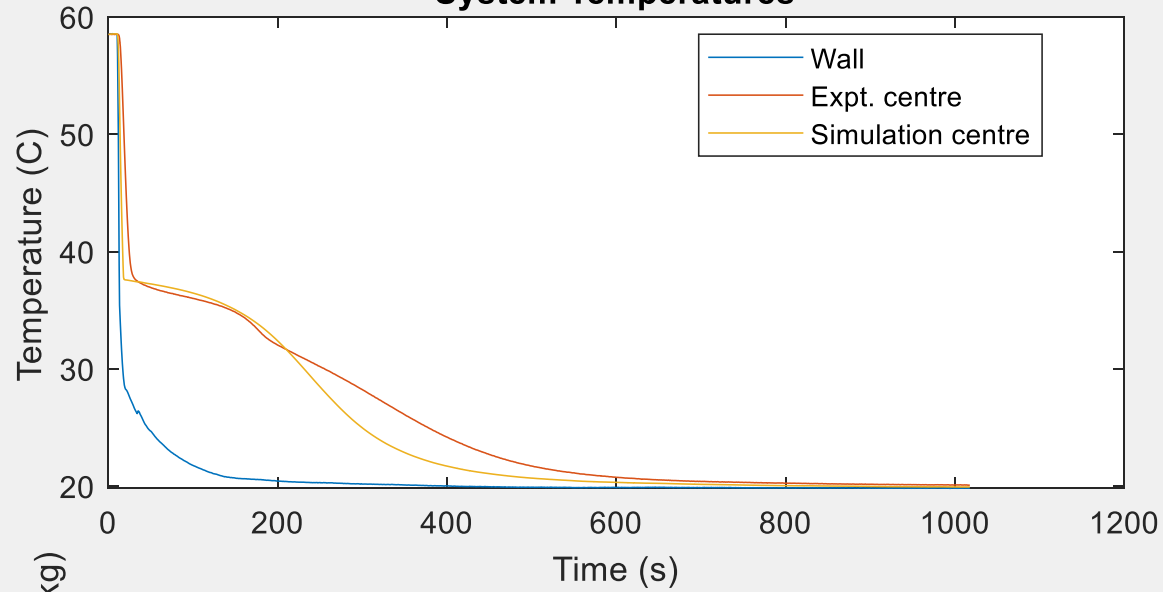


Barium Chloride 2bar LTJ test

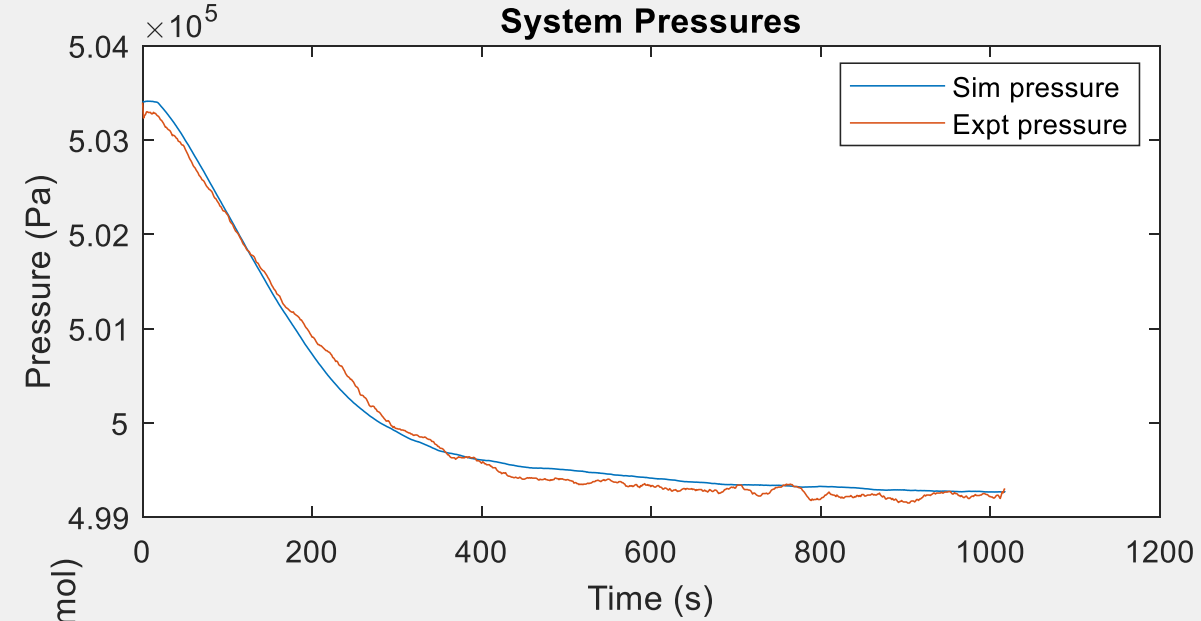


Barium Chloride 5bar LTJ adsorption test

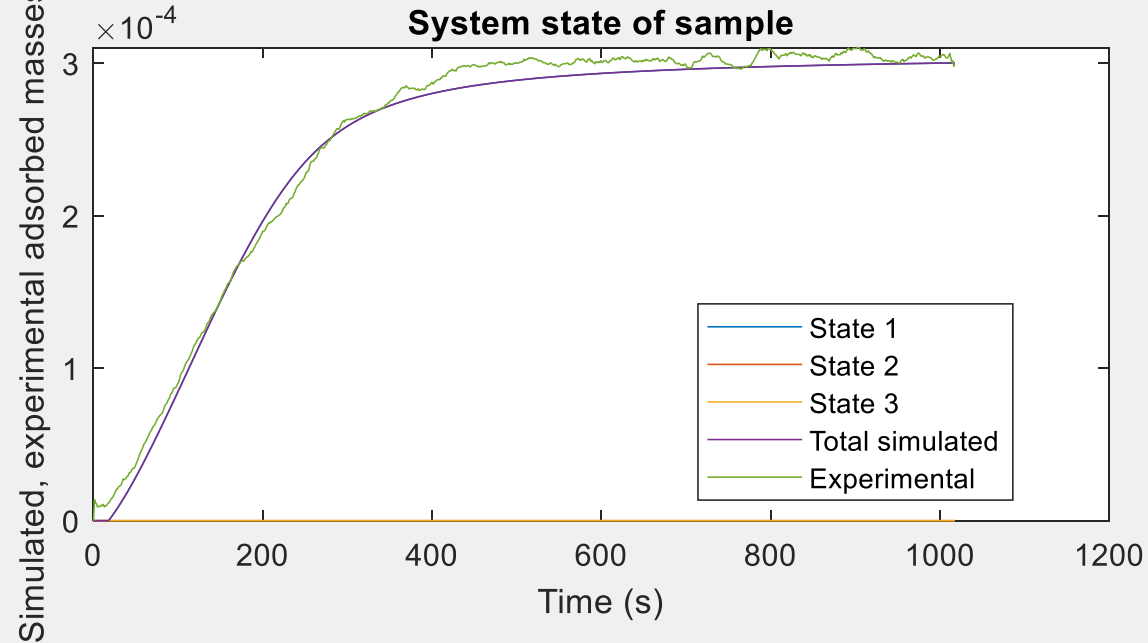
System Temperatures



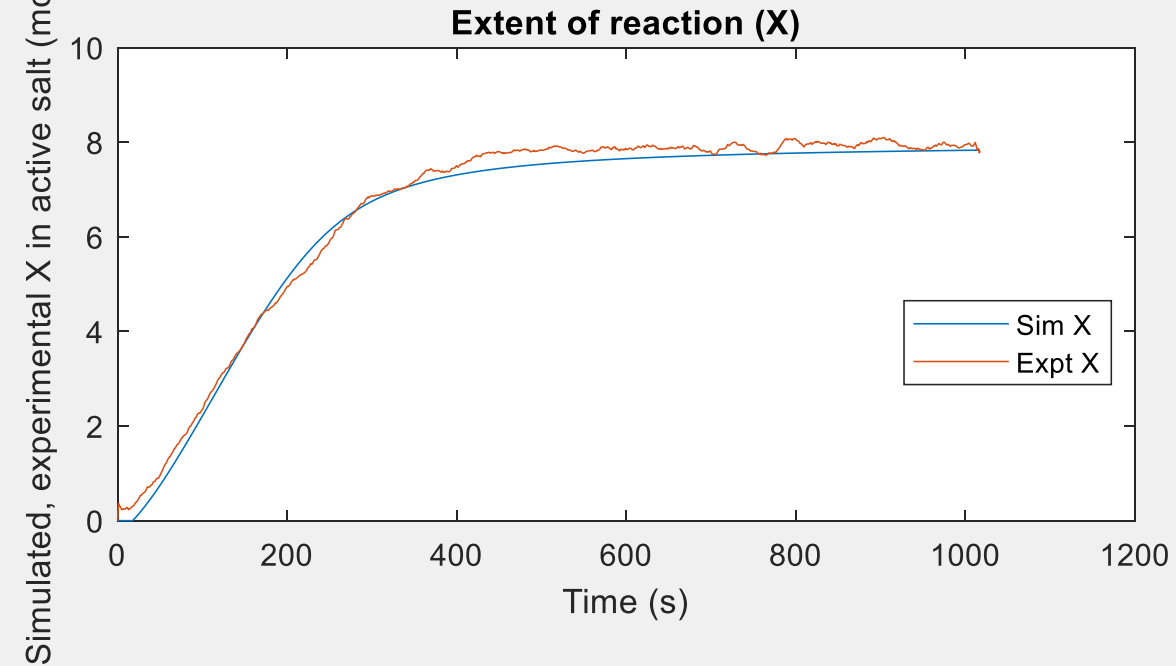
System Pressures



System state of sample

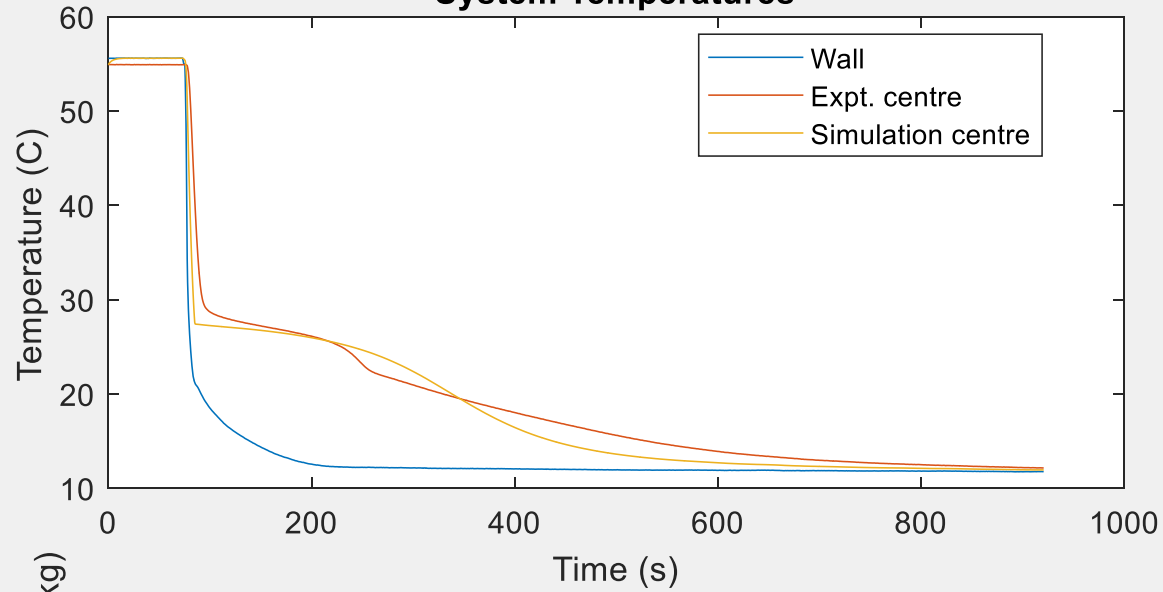


Extent of reaction (X)

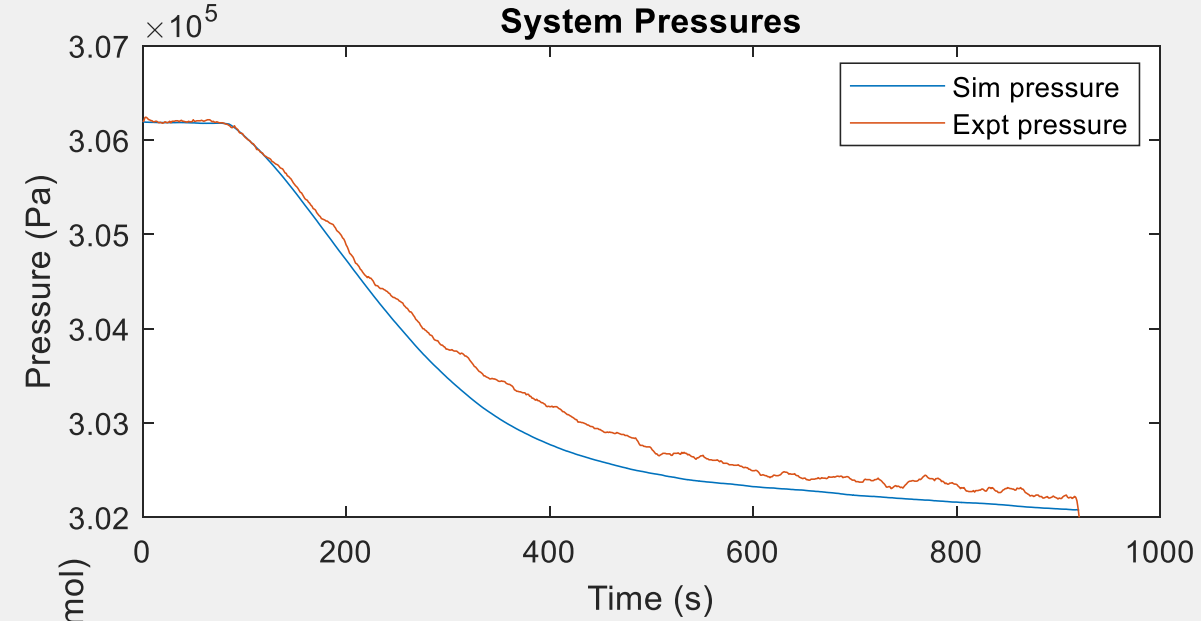


Barium Chloride 3bar LTJ adsorption test

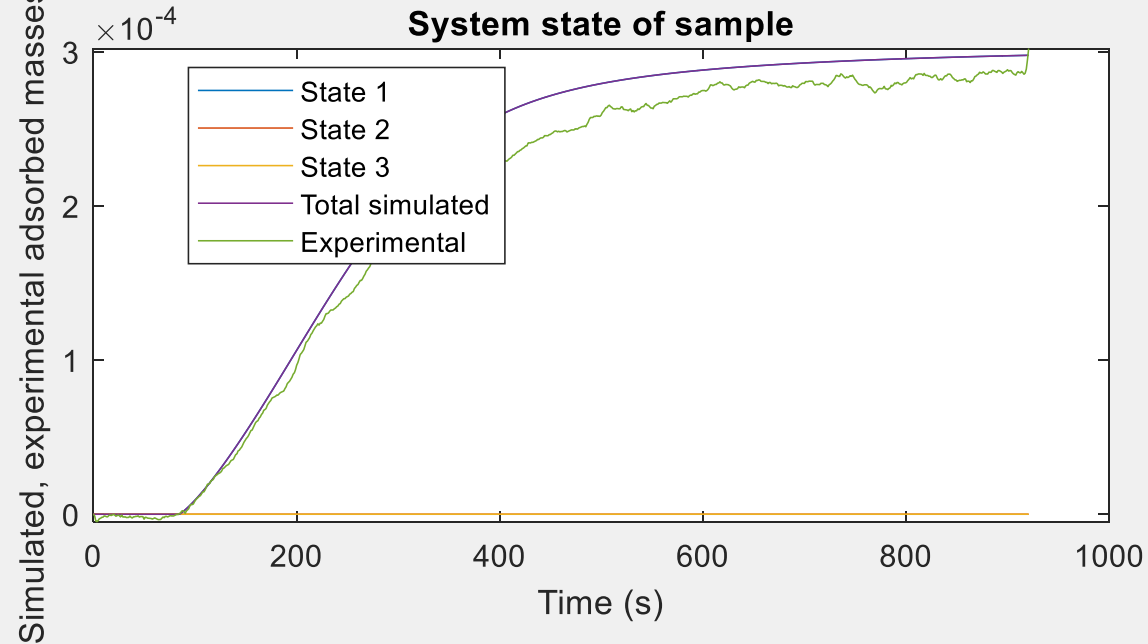
System Temperatures



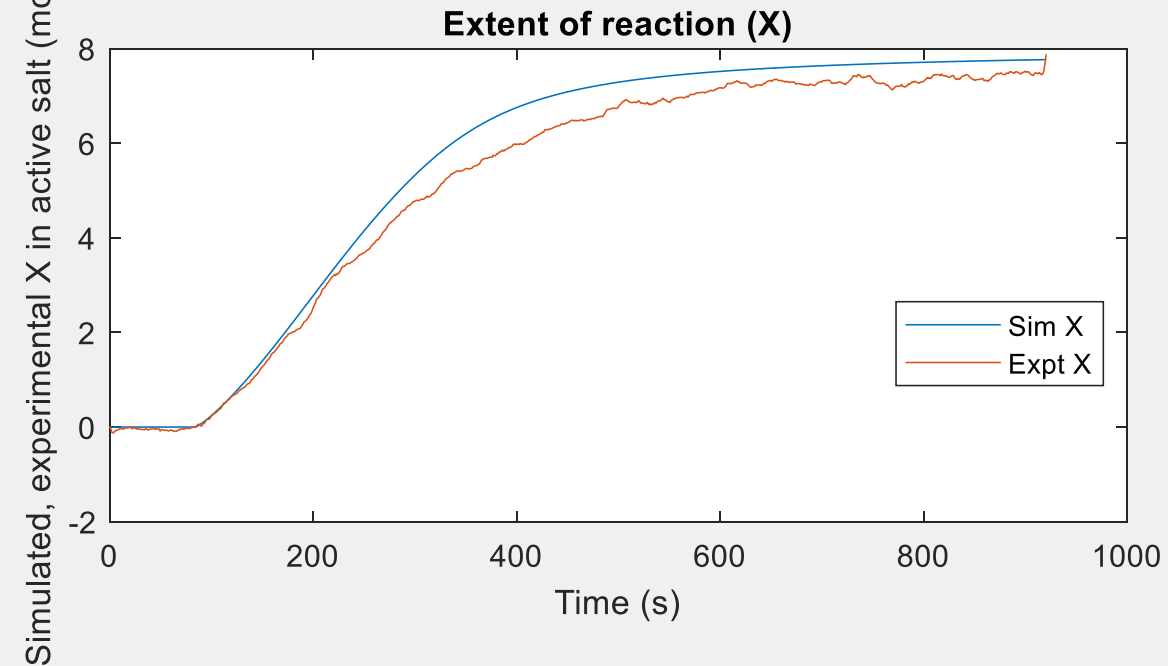
System Pressures



System state of sample

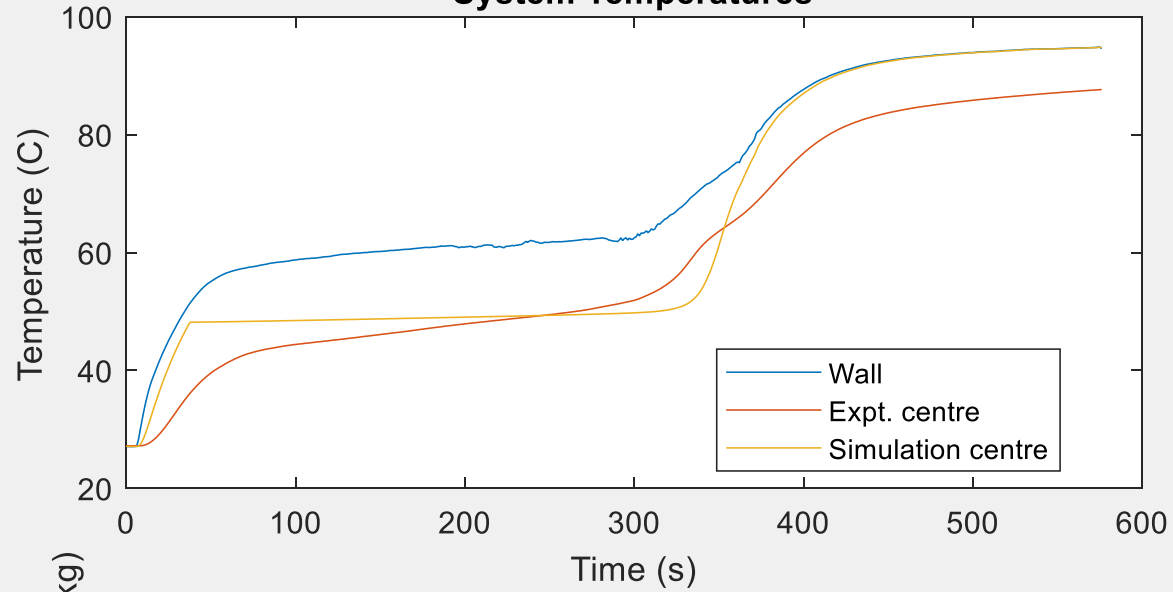


Extent of reaction (X)

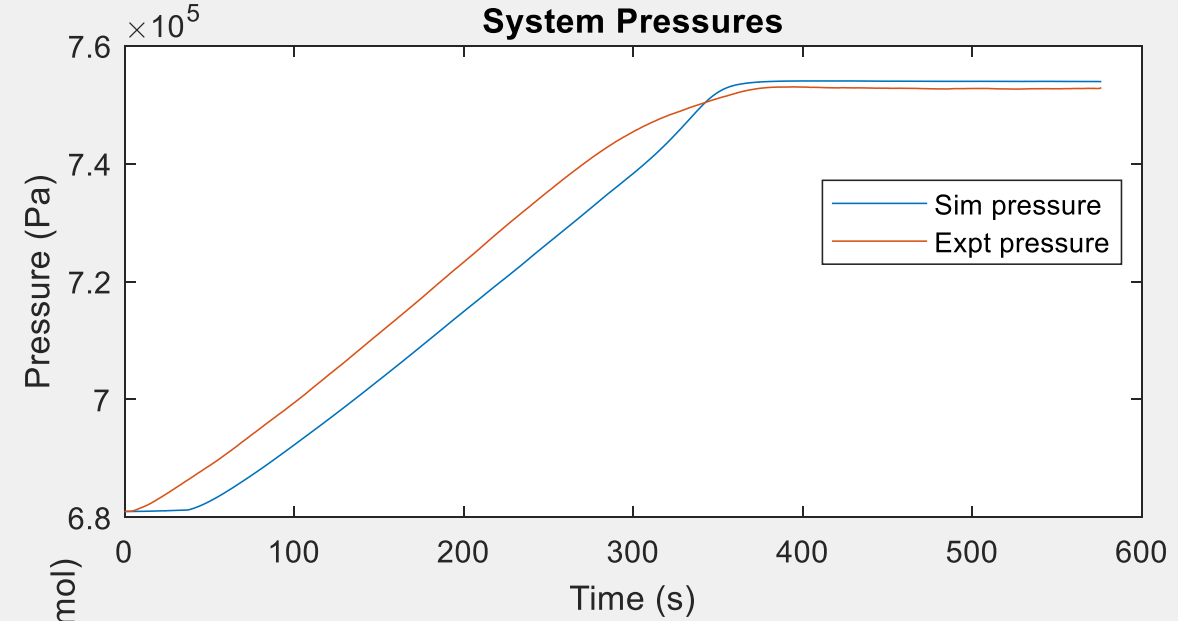


Barium Chloride Shell LTJ test

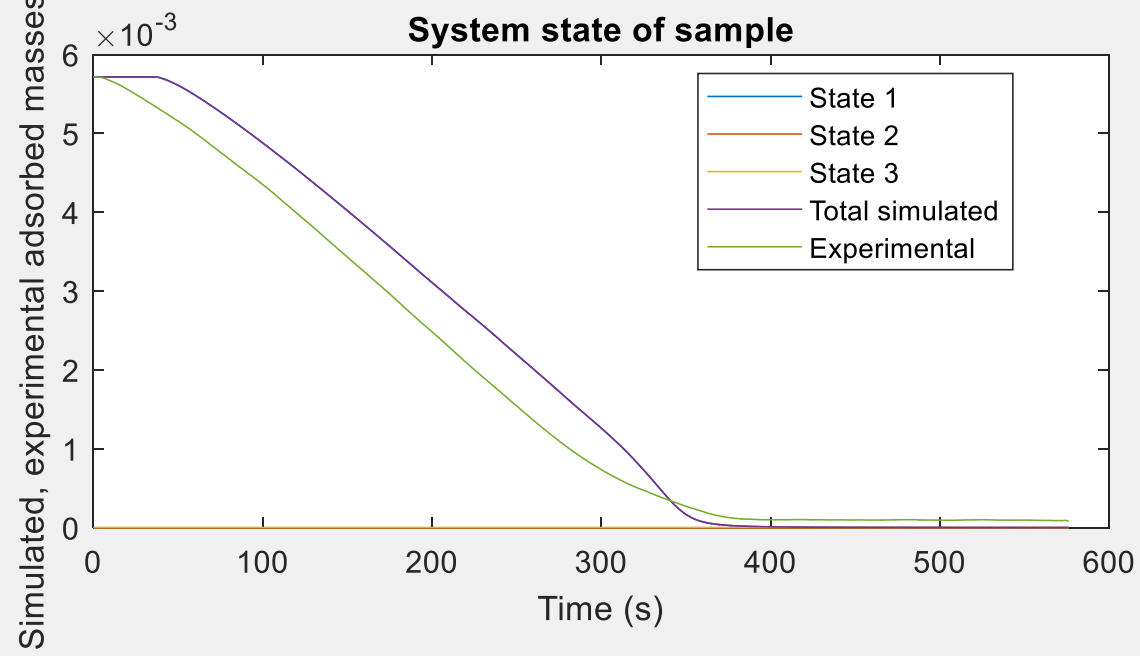
System Temperatures



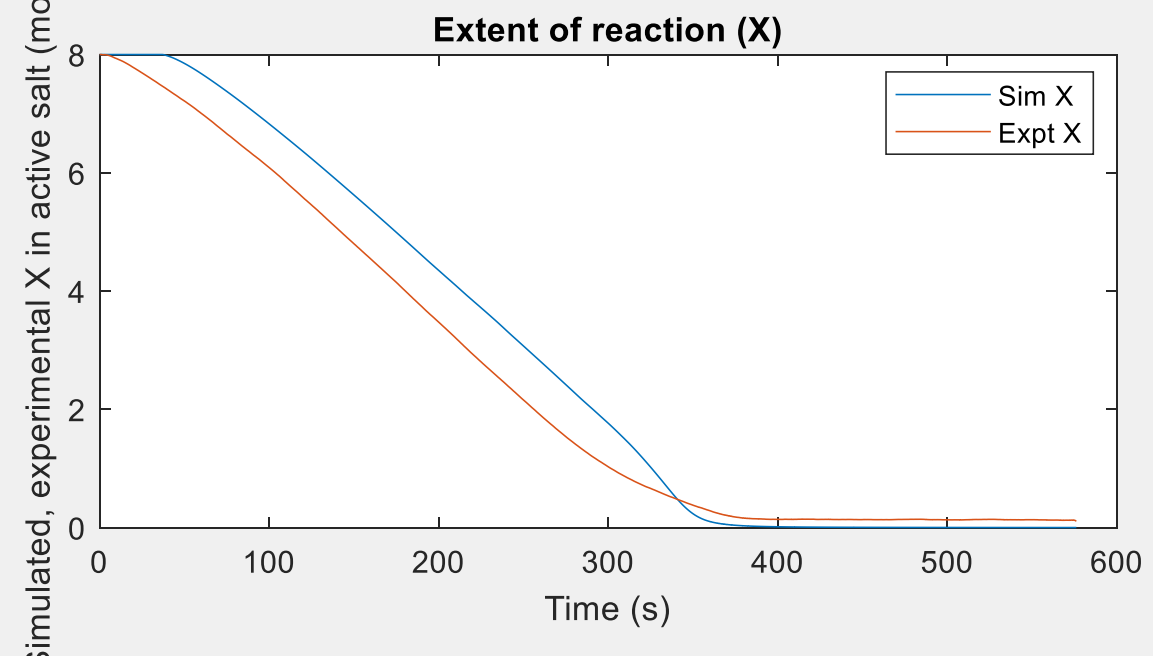
System Pressures



System state of sample



Extent of reaction (X)



To conclude

- Model is predicting well and keen to discuss this
- Also would be pleased for any insight into the salts deviant behaviour
- From the results it is possible to work out a (peak) power/volume value and use this as a basis for designing a machine

Thank you for listening

Any questions?

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