

# Ammonia-Salt Research at Warwick

MI meeting

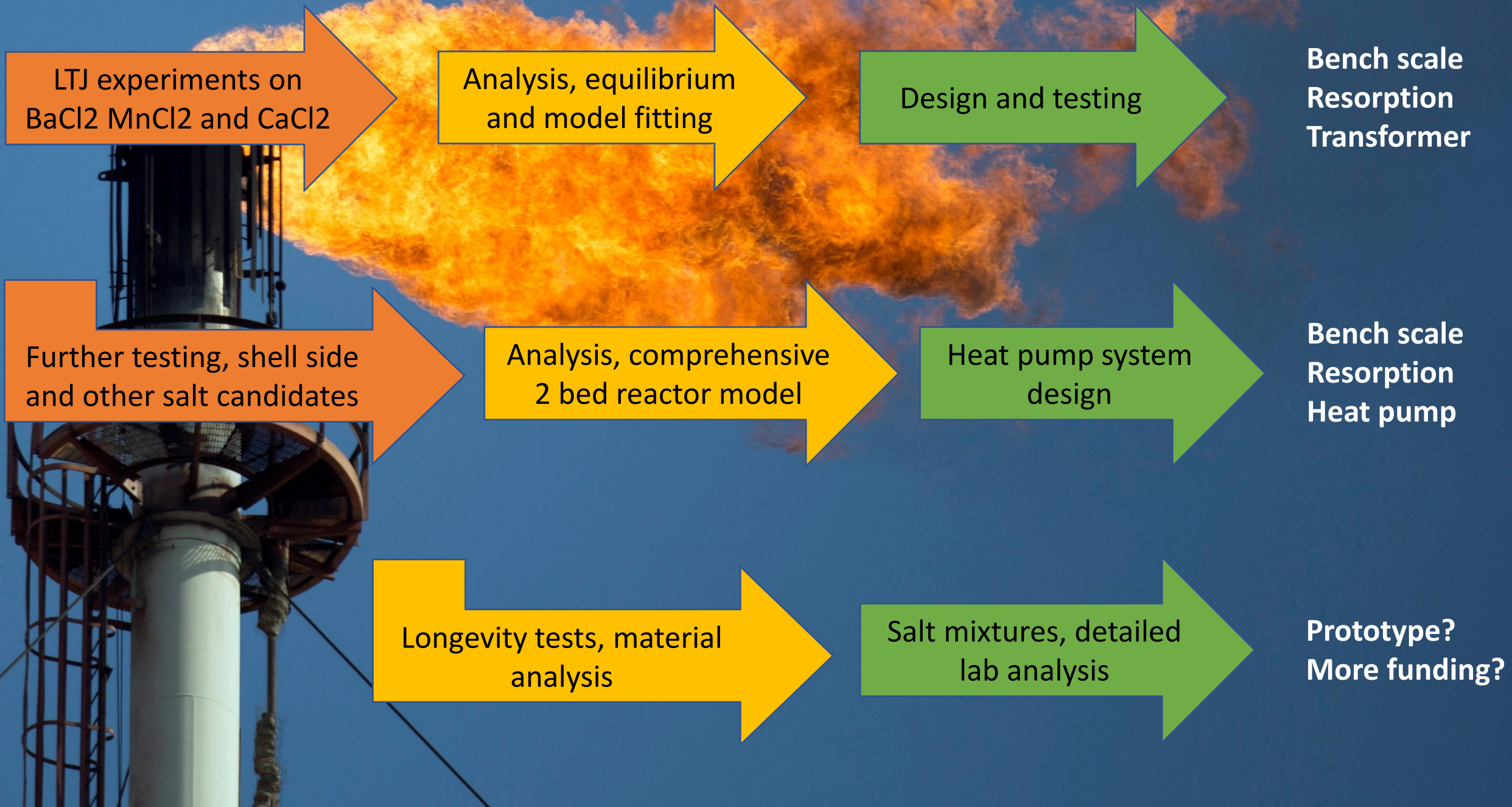
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8<sup>th</sup> October 2020

**ERA** ENERGY  
RESEARCH  
ACCELERATOR

**EPSRC**  
Engineering and Physical Sciences  
Research Council

**WARWICK**  
THE UNIVERSITY OF WARWICK



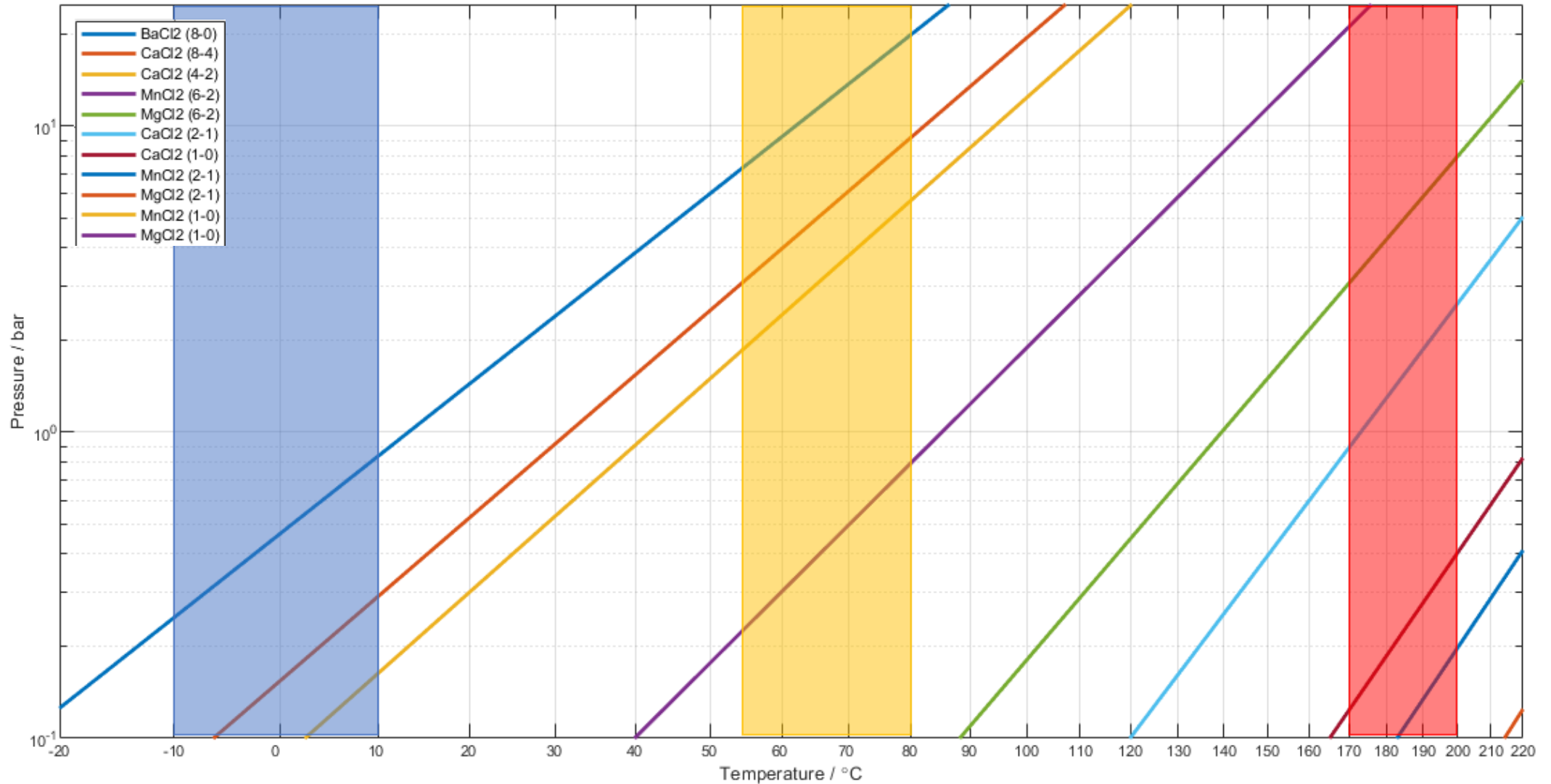
External heat input at  $T_L$



Delivery heat output at  $T_M$

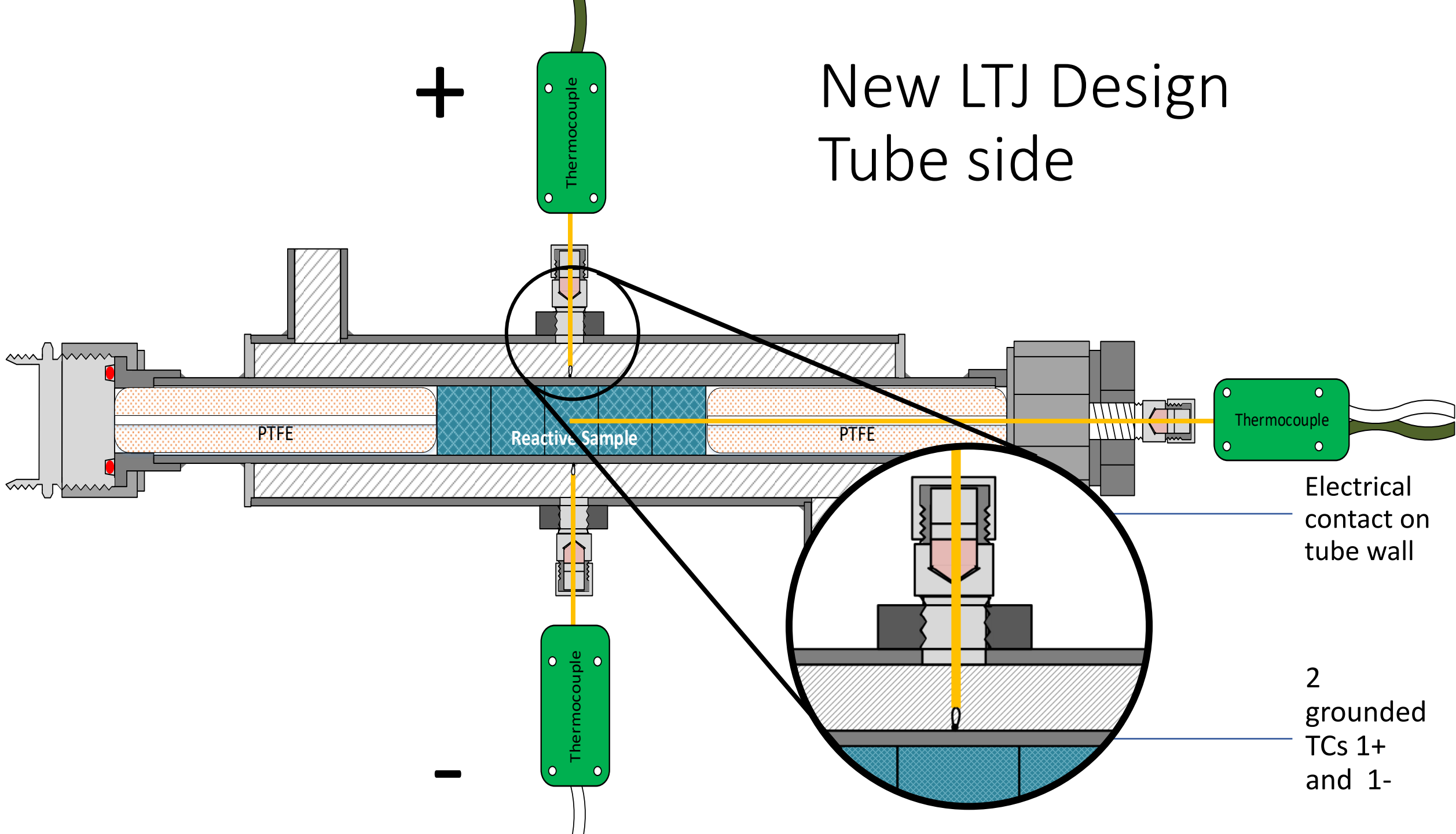


Heat input at  $T_H$



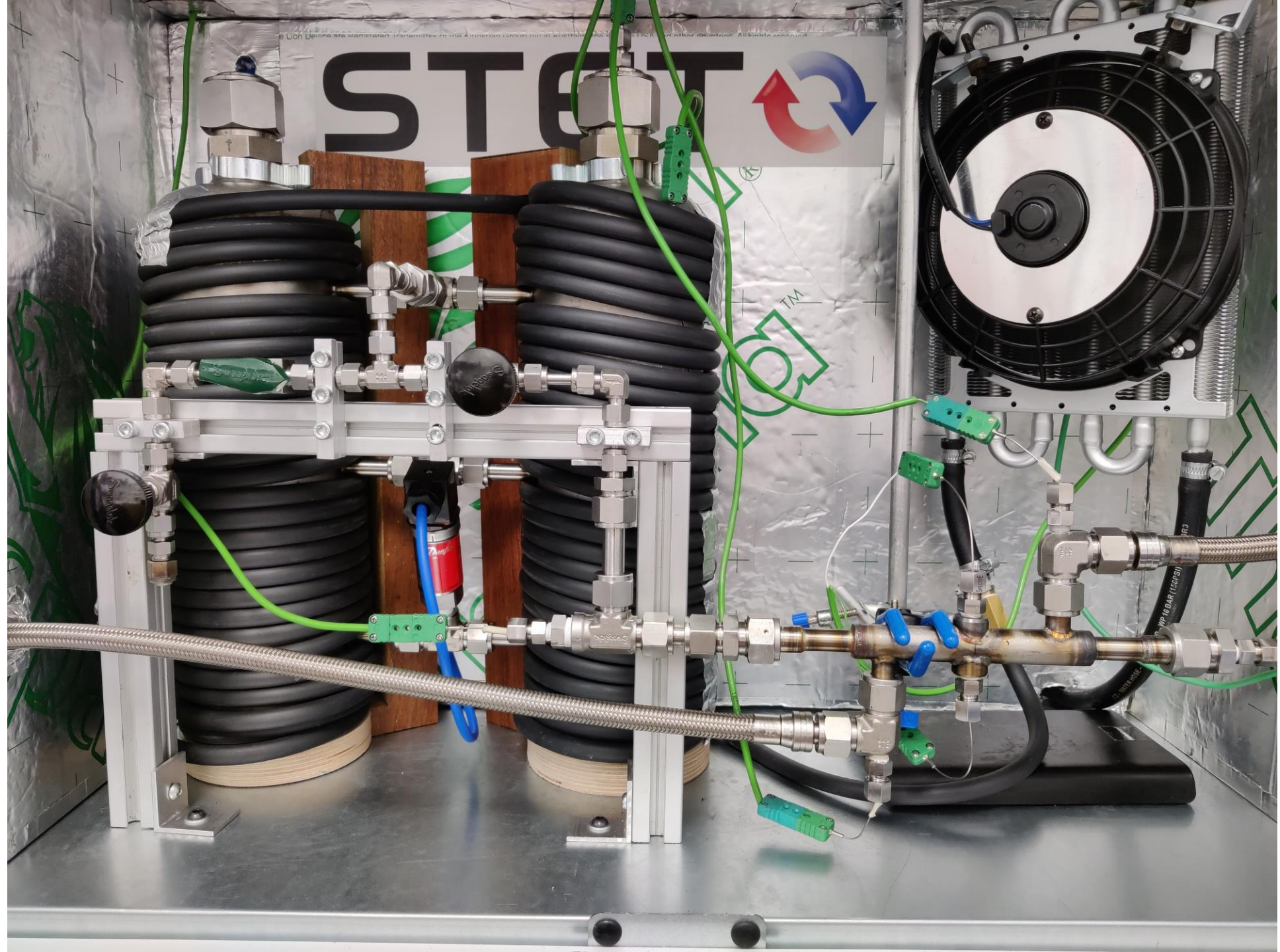
BaCl<sub>2</sub> (LTS) with MnCl<sub>2</sub> as HTS. LTJ performance of LP BaCl<sub>2</sub> currently ongoing.  
Other salt pairings to be considered based on results.

# New LTJ Design Tube side



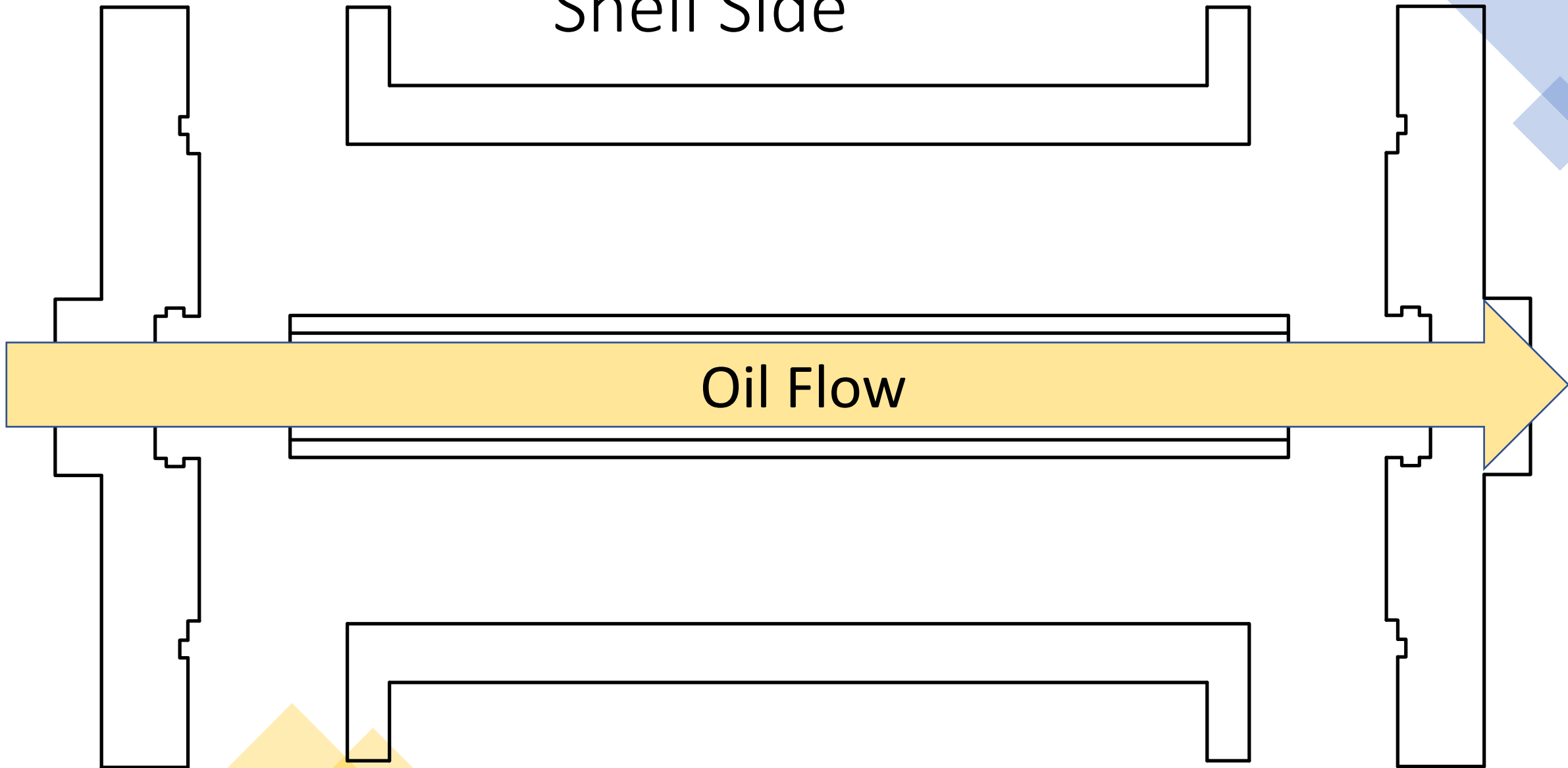
Electrical contact on tube wall

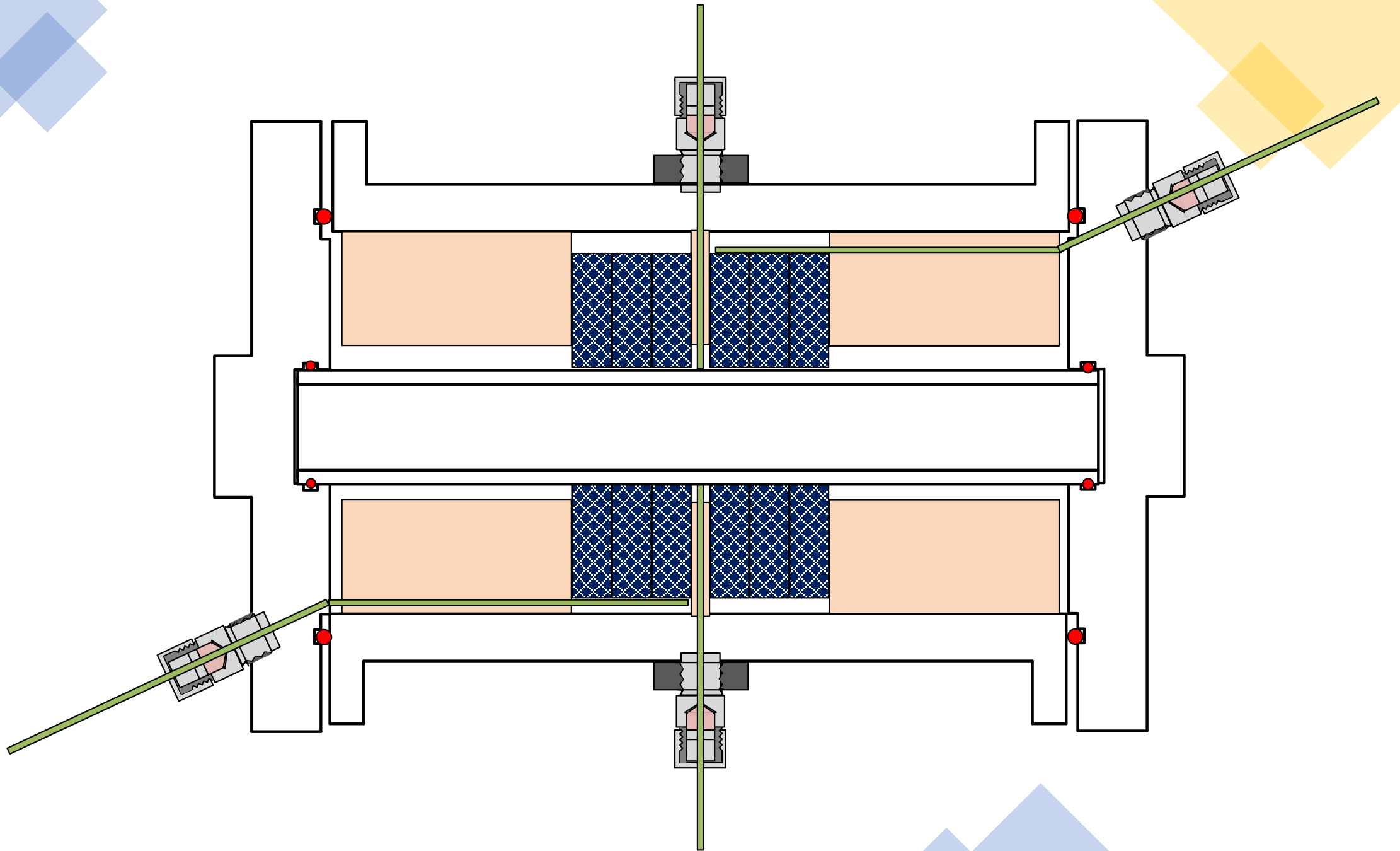
2 grounded TCs 1+ and 1-



Shell Side

Oil Flow

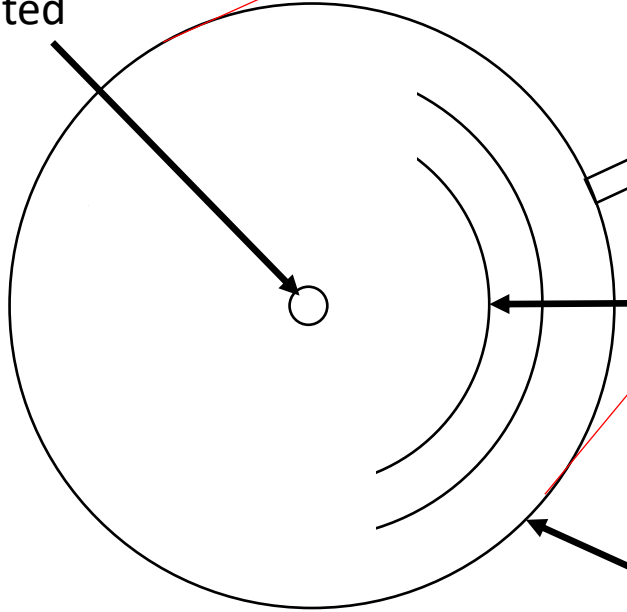




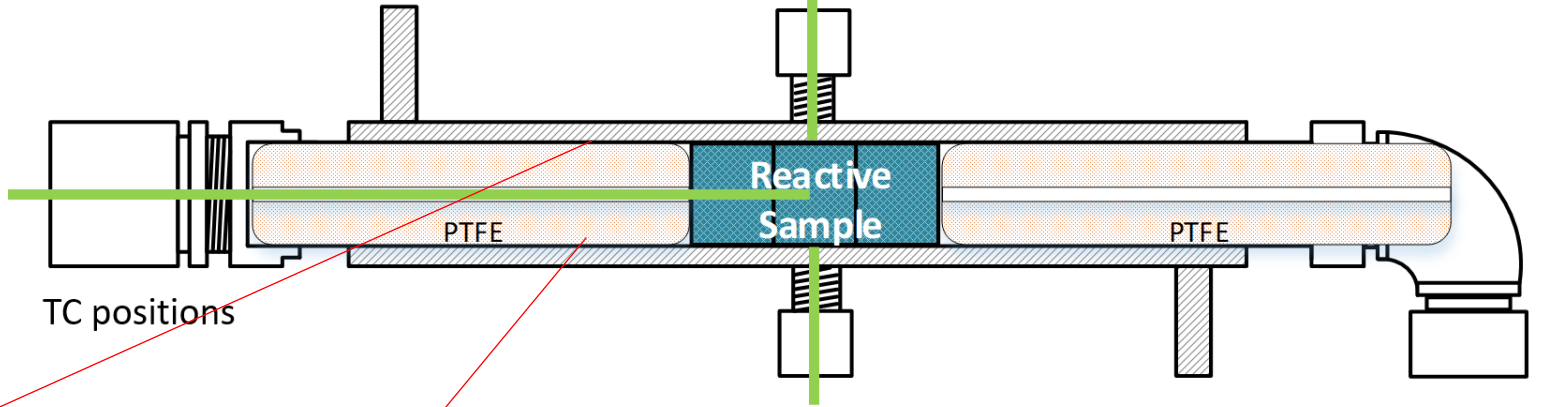
# LTJ Test modelling

## 1-D axi-symmetric model

Centre thermocouple temperature to be simulated



## Large Temperature Jump Reactor



TC positions

½ inch pipe centre

1 inch pipe jacket

PTFE to fill heated volume

O-ring Swagelok face seal fitting

$p$  Pressure to be simulated

$n$  elements of ENG and salt at radius  $r$

Wall at measured temperature (boundary condition)



# Rate equations (2 reactions):

$m_{ads\ 1}$	$m_{ads\ 2}$	$m_{ads\ 3}$
$m_{salt\ 1}$	$m_{salt\ 2}$	$m_{salt\ 3}$

**Time  $t$**

State 1 = .A mols  $\text{NH}_3$     State 2 = .B mols  $\text{NH}_3$     State 3 = .C mols  $\text{NH}_3$

Define:

$dm_{salt\ 12}$  = mass converted State 1 to State2

$dm_{salt\ 23}$  = mass converted State 2 to State3

$dm_{gas\ 12}$  = mass of gas desorbed from State 1 to State2

$dm_{gas\ 23}$  = mass of gas desorbed from State 2 to State3

Use chemists' rate formula:

$$\frac{dX}{dt} = (1 - X)^y A \frac{p_{eq} - p}{p}$$

assuming that converting phases unaffected by third phase, then:

Reaction 12 (desorbing):

$$dm_{salt\ 12} = (m_{salt\ 1} + m_{salt\ 2}) dt \left( \frac{m_{salt\ 1}}{m_{salt\ 1} + m_{salt\ 2}} \right)^{y_{12}} A_{12} \frac{p_{eq\ 12} - p}{p}$$

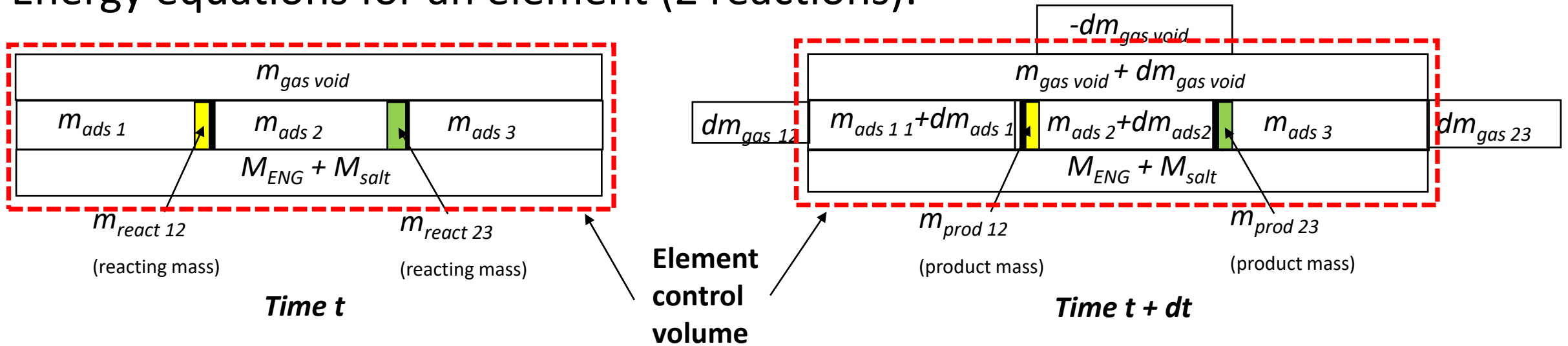
Reaction 23 (desorbing):

$$dm_{salt\ 23} = (m_{salt\ 2} + m_{salt\ 3}) dt \left( \frac{m_{salt\ 2}}{m_{salt\ 2} + m_{salt\ 3}} \right)^{y_{23}} A_{23} \frac{p_{eq\ 23} - p}{p}$$

$m_{ads\ 1} + dm_{ads\ 1}$	$m_{ads\ 2} + dm_{ads\ 2}$	$m_{ads\ 3} + dm_{ads\ 3}$
$m_{salt\ 1} + dm_{salt\ 1}$	$m_{salt\ 2} + dm_{salt\ 2}$	$m_{salt\ 3} + dm_{salt\ 3}$

**Time  $t + dt$**

# Energy equations for an element (2 reactions):



First Law for element control volume

$$dQ = \Delta U_{ENG} + \Delta U_{salt} + \Delta U_{ads} + \Delta U_{gas\ void} + dm_{gas\ 12} h_{out} + dm_{gas\ 23} h_{out} - dm_{gas\ void} h_{out}$$

[Desorption  $dm_{gas}$  is positive out and  $h_{out}$  is at element temperature

Adsorption  $dm_{gas}$  is negative and  $h_{out}$  is at reservoir temperature]

After much manipulation, for desorbing:

$dT$

$$= \frac{dQ - dm_{gas\ 12} \Delta h_{12} - dm_{ads\ 12} p v_{ads} \left(1 - \frac{B}{A}\right) - dm_{gas\ 23} \Delta h_{23} - dm_{ads\ 23} p v_{ads} \left(1 - \frac{C}{B}\right) + V_{void} \frac{dp}{1 + dp/T}}{M c_p + \sum_1^3 m_{ads} c_{v\ ads} + m_{gas\ void} c_{v\ gas} - V_{void} \frac{pT}{1 + dp/T}}$$

# New Matlab code to handle complex models

```
% reactor_sim_1
% This is the top-level script file; everything else uses functions.

% User-edited code to set up
[rig, test] = rsim_parameter

% "rig" defines hardware, "test" defines simulation
% For traceability, both "rig" and "test" are saved
% in test, so to re-run the simulation, use
% rsim_parameters above and test
% Both rig and test can be imported into a new script

%-----
% set derived values
rig = nodal_inputs(rig);
test = filling_mass(rig, test);
%-----
test
```

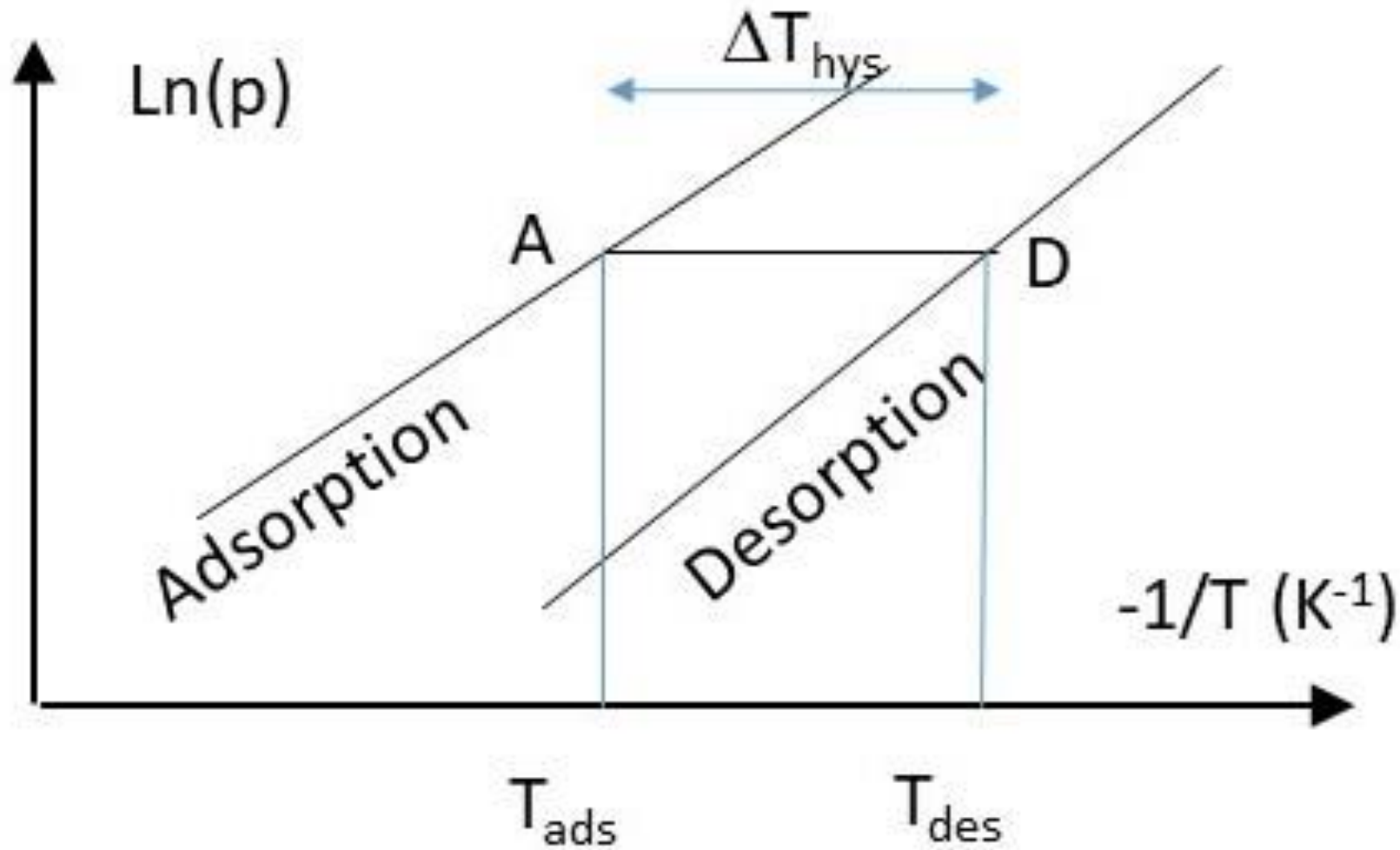
```
rig.Exp_vessel.mc = 4000; % J/K
rig.Exp_vessel.vol = 0.002; % m^3

rig.props.cvNH3ads = 3120; % J/kg NH3, guess???
rig.props.cpGas = 2760; % J/kgK ammonia
rig.props.cENG = 720; % J/kgK
.
.
iR = 1;
rig.Reactor(iR).gVol = 0.5E-3; % m3
rig.Reactor(iR).iG = logical([0 1]); % gas to outside
rig.Reactor(iR).m = 0; % linear
rig.Reactor(iR).mcp = 20e3; % water pipe m*c
```

- Any number of reactors
- Any number of salts (assumed independent)
- Any number of reactions per salt
- 1D  $(x,t)$  flat or  $(r,t)$  cylindrical – could extend to 2D
- Allows non-uniform grids (Fornberg's algorithm)
- Uses Matlab's linked ODE solver for "Method of Lines" solution and structured variables for clarity

```
/mol of NH3 changing state, ads/des
J/molK ditto
```

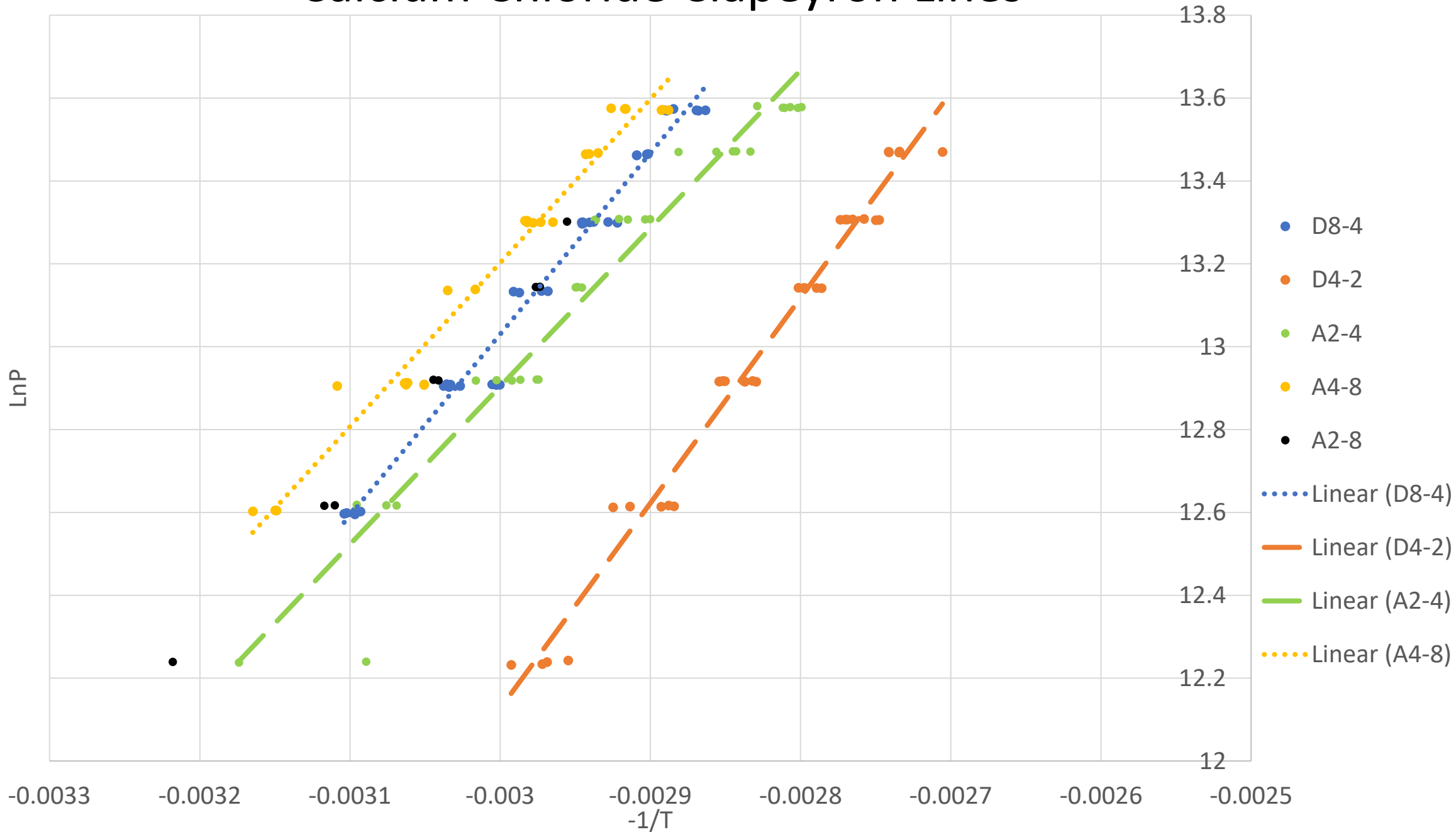
```
rig.Reactor(iR).salt = salt;
```



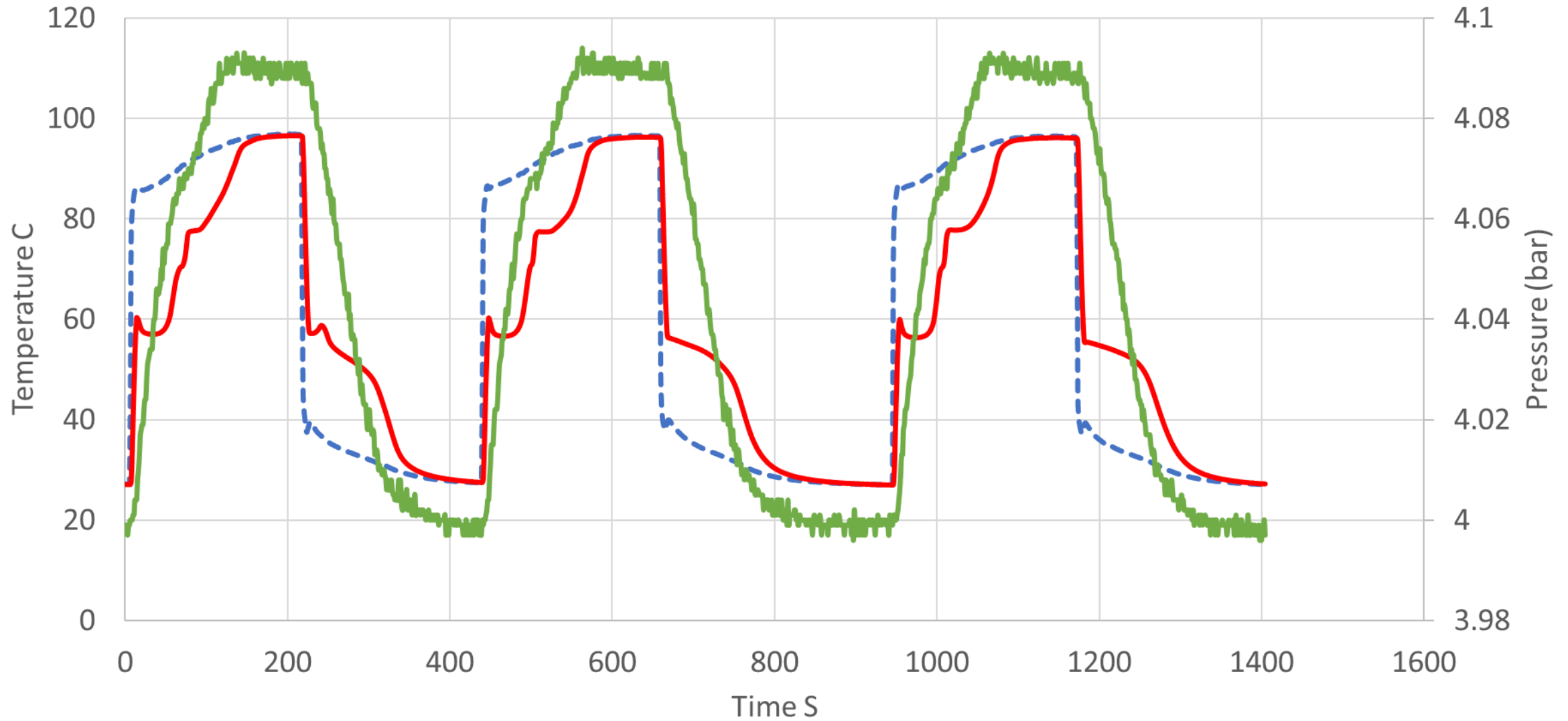
$$\Delta H_{ads} = \Delta H_{des} + \Delta T_{hys} (c_{v ads} - c_{v gas})$$

$$\ln(p_{ads}) = \frac{\Delta S_{ads}}{R} - \frac{\Delta H_{ads}}{R(T_{des} - \Delta T_{hys})}$$

# Calcium Chloride Clapeyron Lines



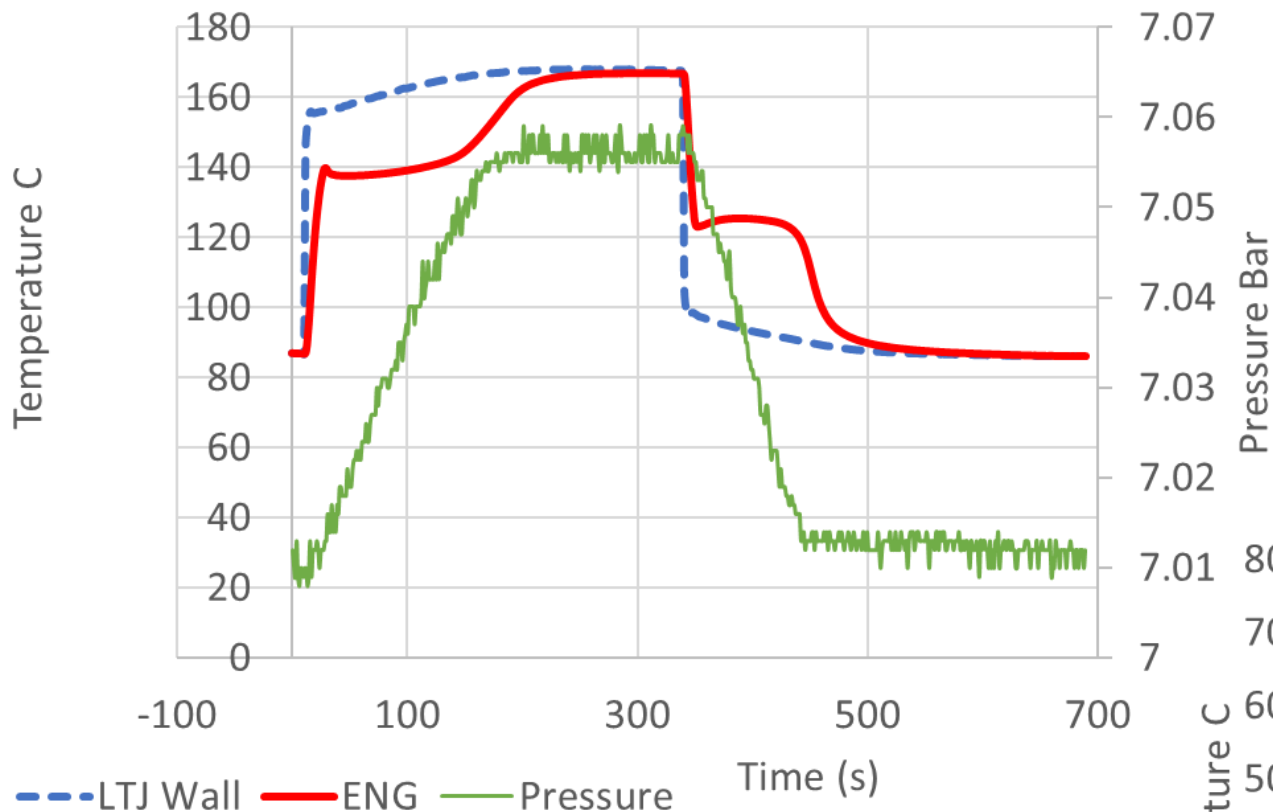
# Calcium Chloride Large Temperature Jump Cycles



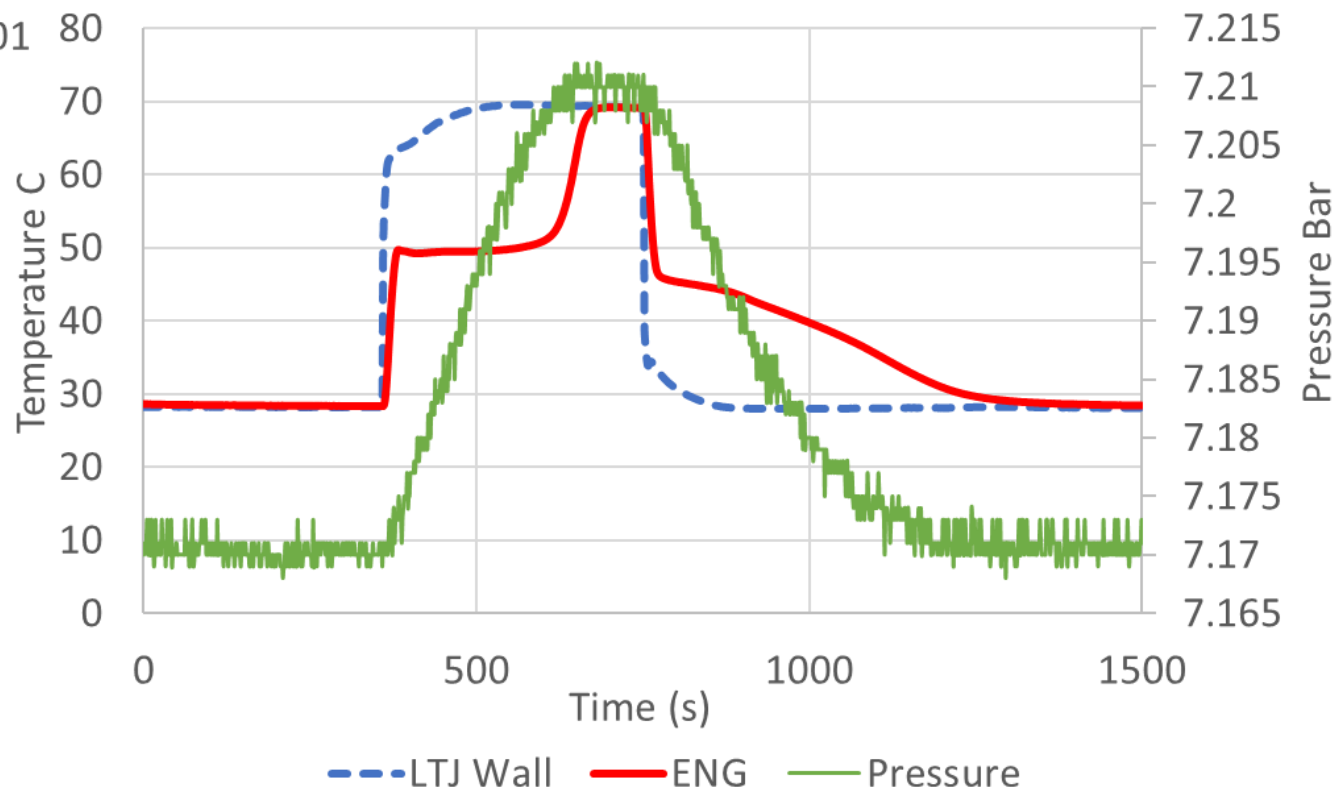
Two stage phase changes

--- LTJ Wall    — ENG    — Pressure

### Manganese Chloride



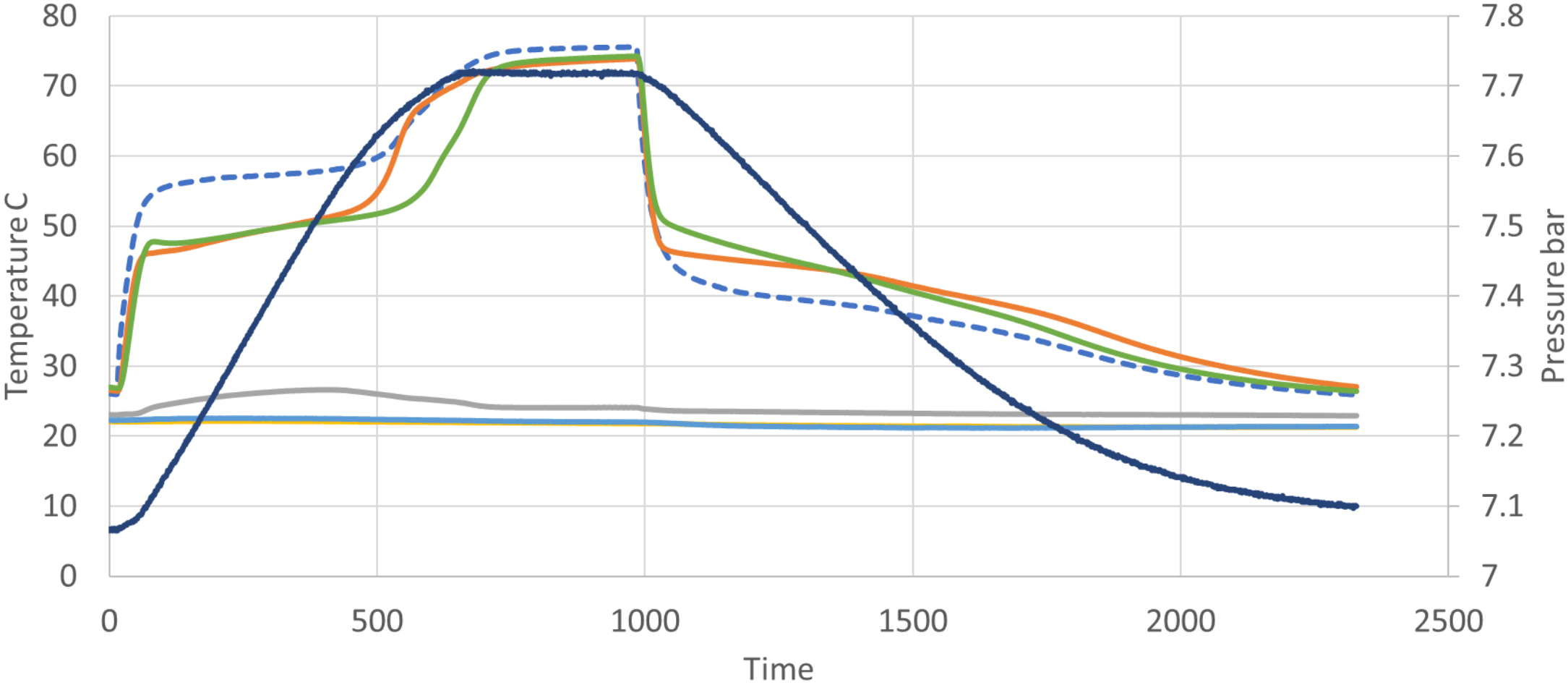
### Barium Chloride



Single stage phase changes

# Single stage phase change

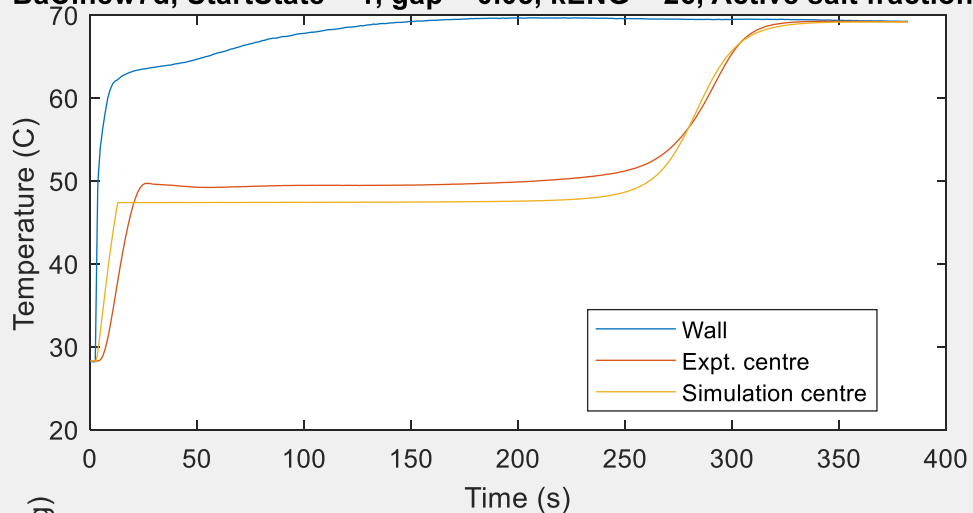
Shell Side Barium Chloride



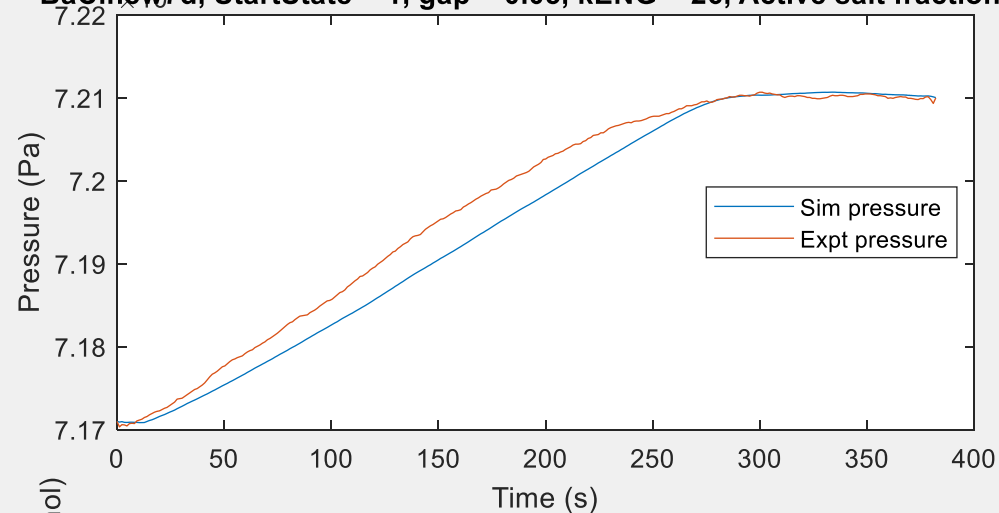
--- LTJ PipeW    — ENG Top    — Pipework    — Exp V Wall    — Exp V    — ENG Bottom    — Pressure



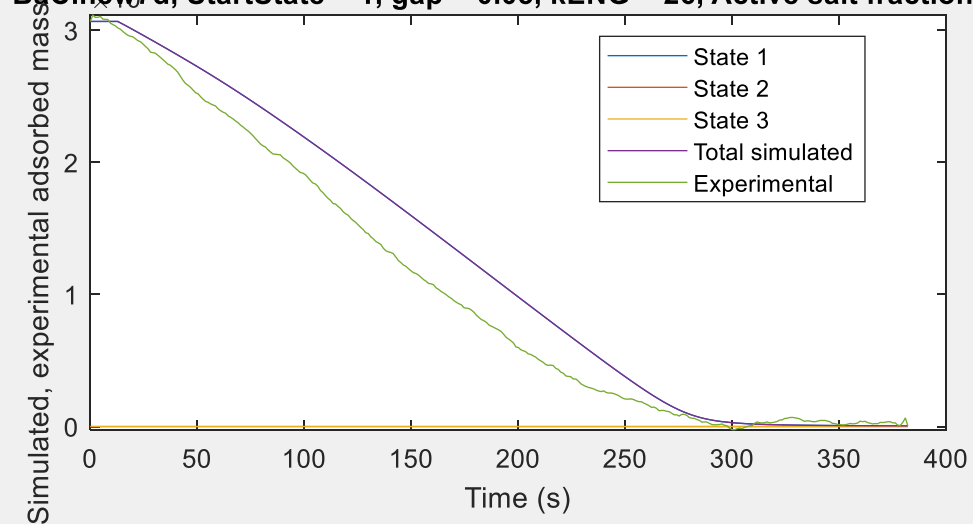
**BaClnew7d, StartState = 1, gap = 0.05, kENG = 26, Active salt fraction 0.8**



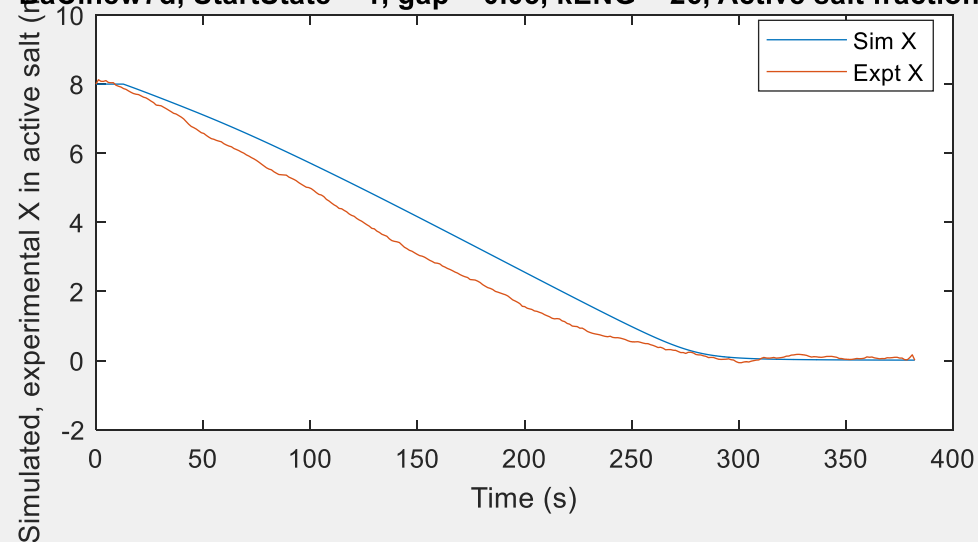
**BaClnew7d, StartState = 1, gap = 0.05, kENG = 26, Active salt fraction 0.8**



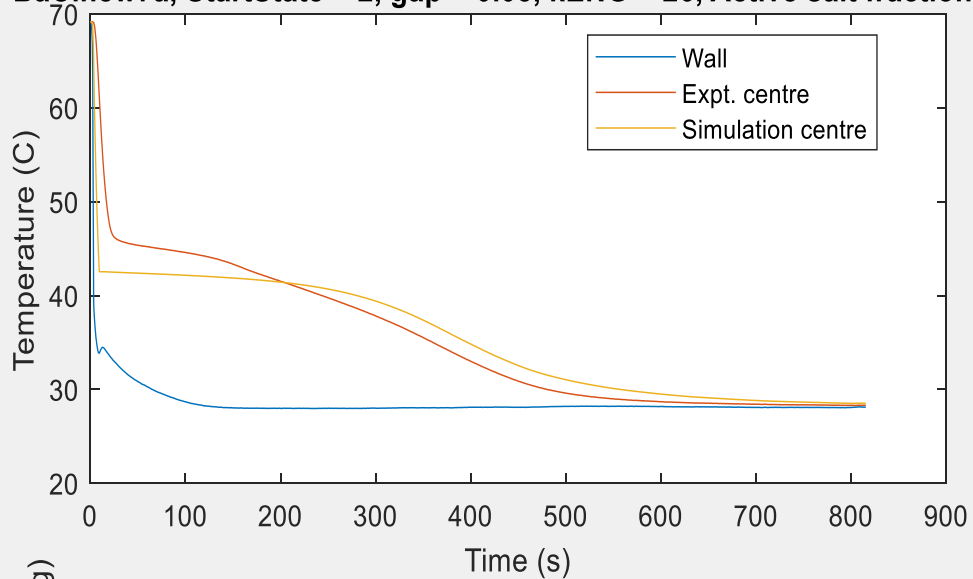
**BaClnew7d, StartState = 1, gap = 0.05, kENG = 26, Active salt fraction 0.8**



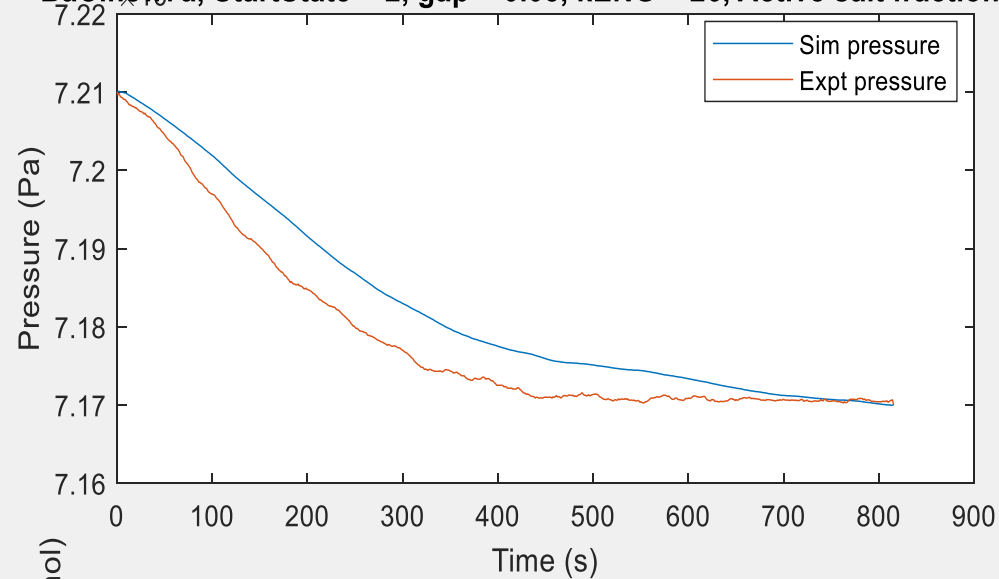
**BaClnew7d, StartState = 1, gap = 0.05, kENG = 26, Active salt fraction 0.8**



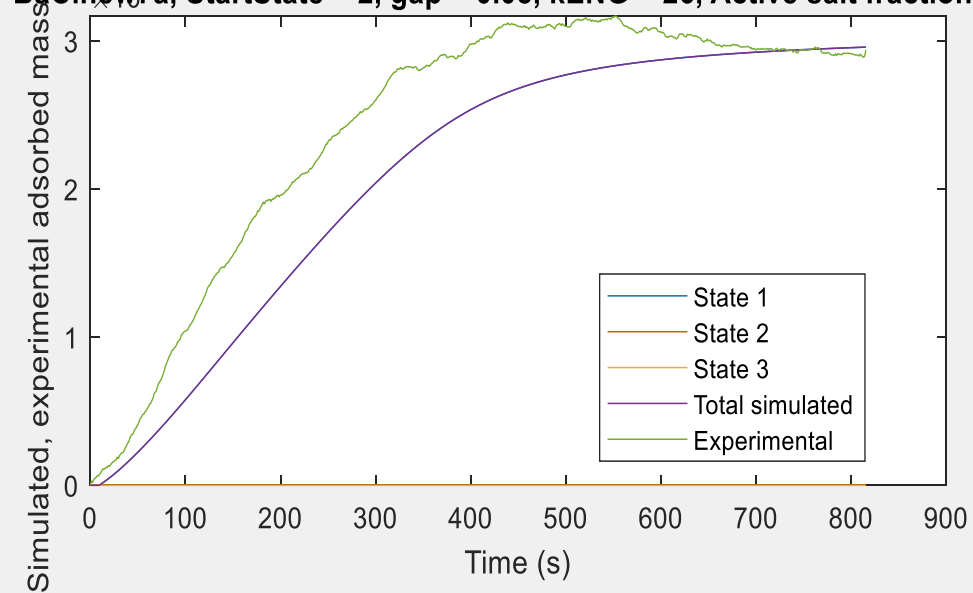
**BaCInew7a, StartState = 2, gap = 0.05, kENG = 26, Active salt fraction 0.8**



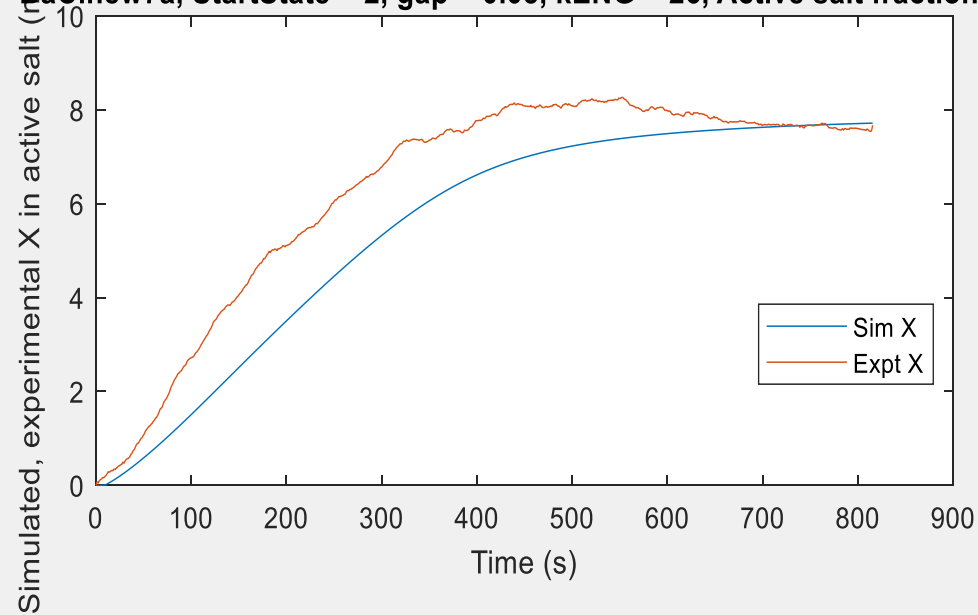
**BaCInew7a, StartState = 2, gap = 0.05, kENG = 26, Active salt fraction 0.8**



**BaCInew7a, StartState = 2, gap = 0.05, kENG = 26, Active salt fraction 0.8**



**BaCInew7a, StartState = 2, gap = 0.05, kENG = 26, Active salt fraction 0.8**



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Thank you for  
listening

